

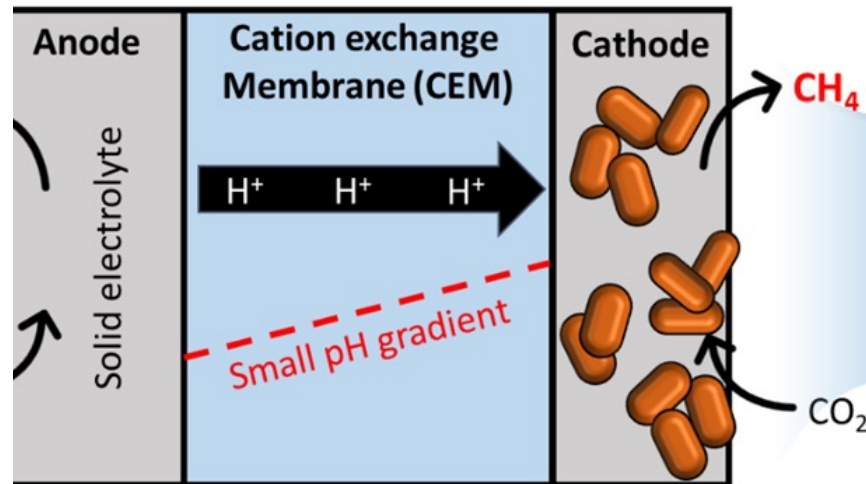
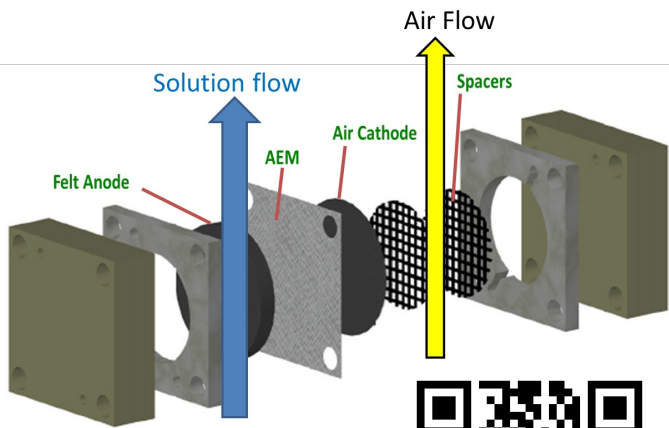
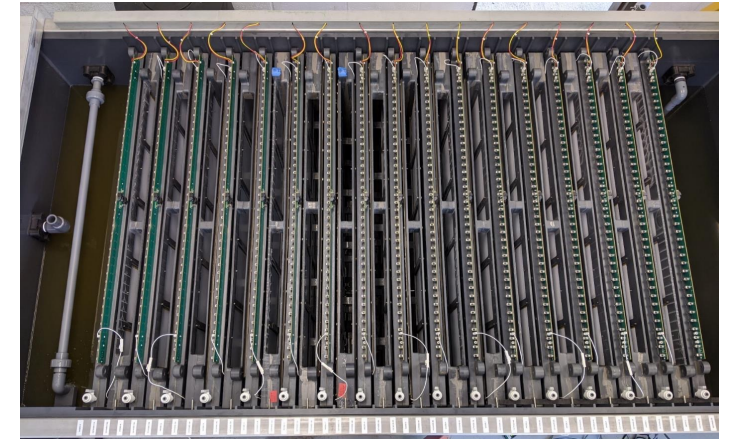
Microbial Electrotechnologies for Converting CO₂ into Natural Gas and Chemicals



Bruce E. Logan

Penn State University, blogan@psu.edu

CORC Carbon Forum
December 7, 2022



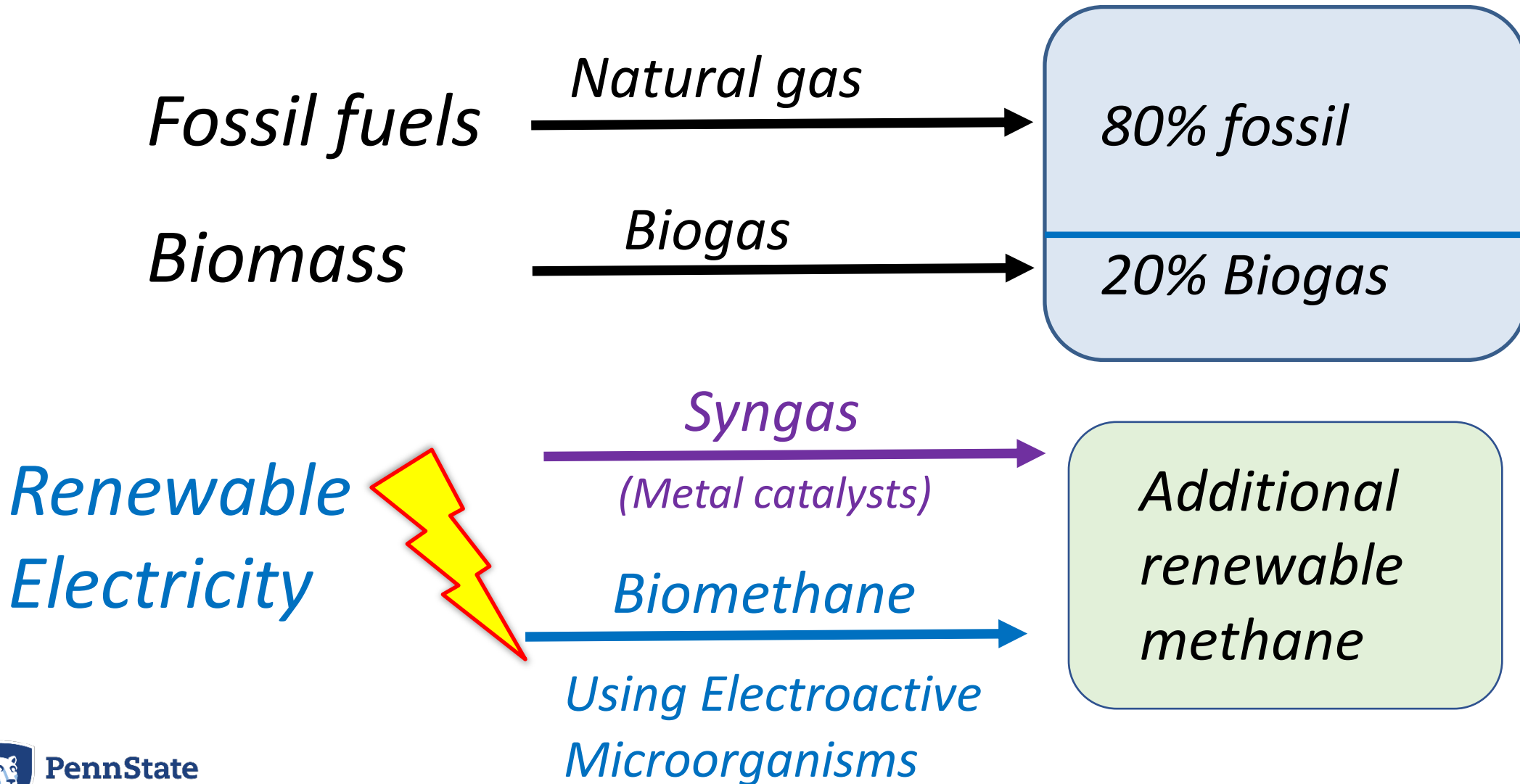
Daily Energy Use
and Carbon Emissions

Fundamentals and Applications for Students
and Professionals

Bruce E. Logan

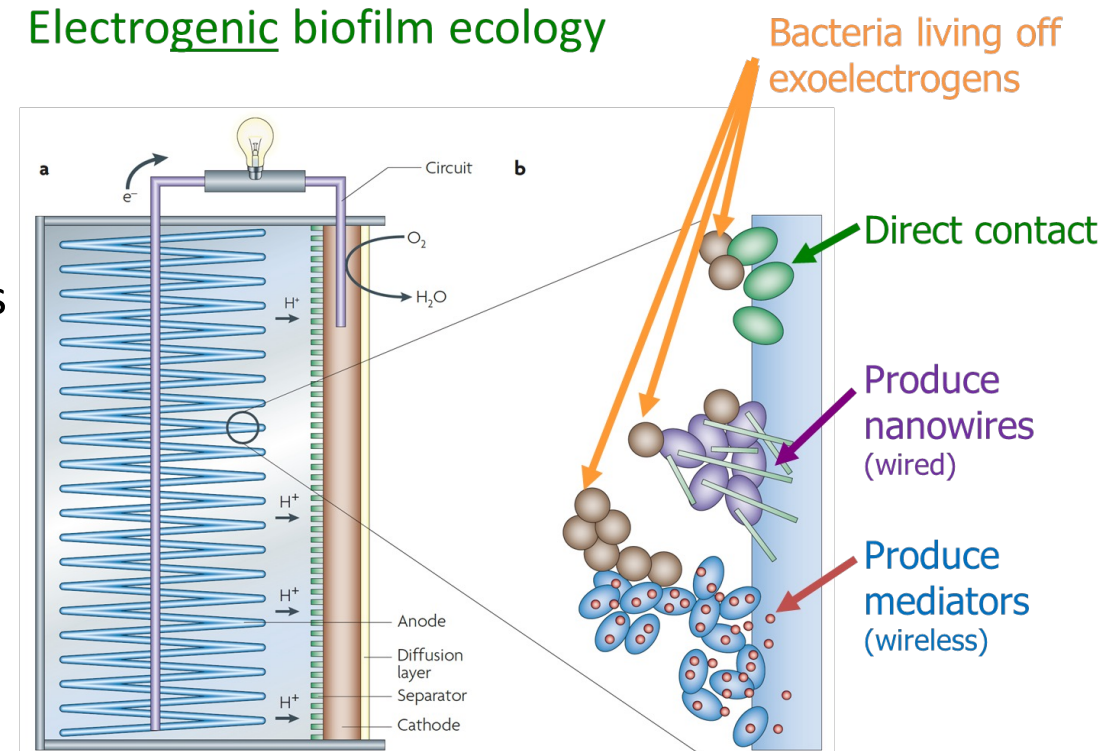


Gas (CH₄) is 16% of Energy use by Denmark



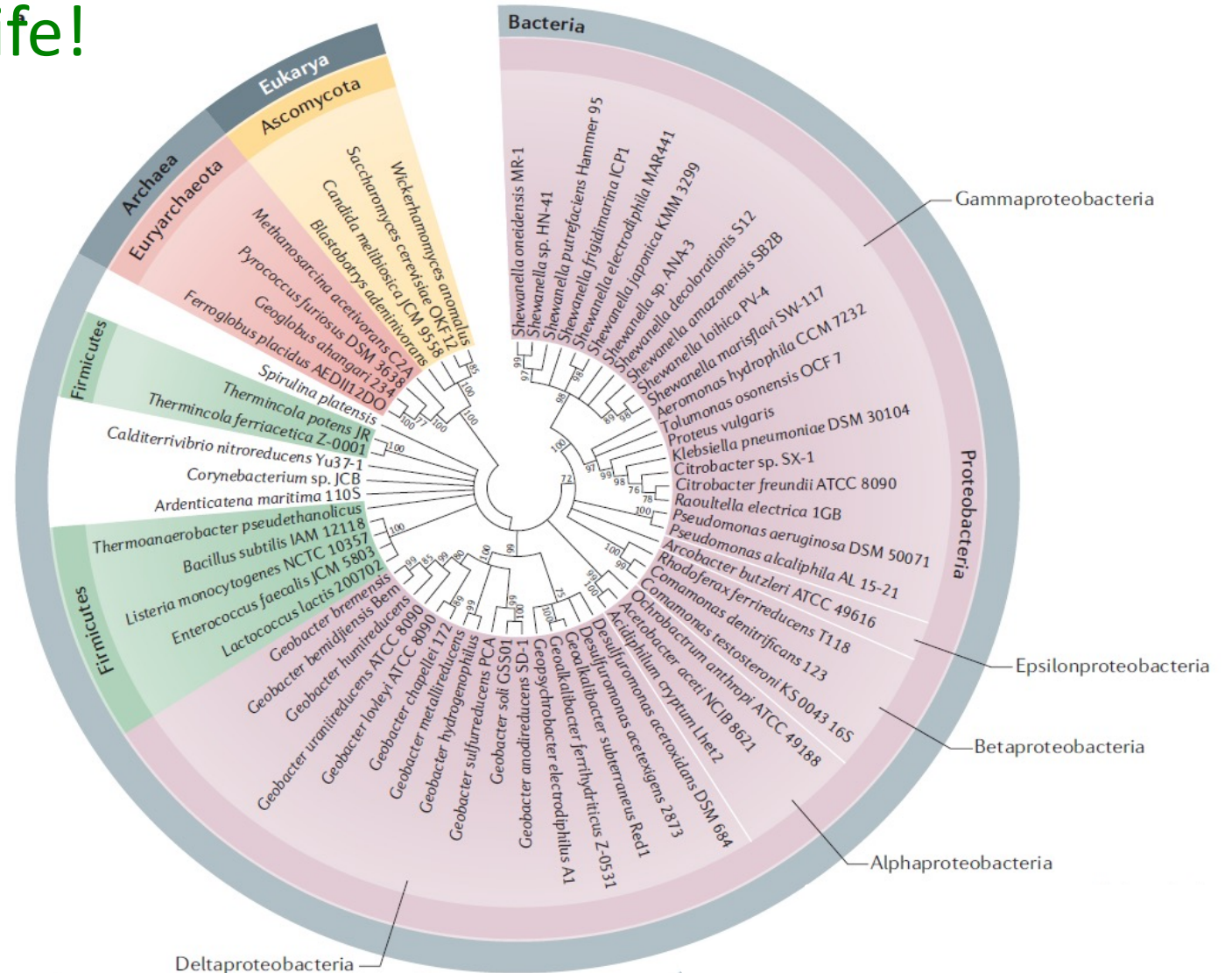
Electroactive microorganisms for Bioelectrochemical Systems

- Exoelectrogenic microorganisms
 - Generate electricity using inorganic (H_2) and simple organic molecules (e.g. acetate)
- Electrotrophic microorganisms
 - Accept electrons and reduce CO_2 to chemical products such as methane (CH_4) and simple organic molecules
- Interspecies electron transfer
 - Electron transfer between two microorganisms of different species
- Bioelectrochemical systems (BES)
 - Use electroactive (electrogenic or electrotrophic) microorganisms in systems with electrodes.



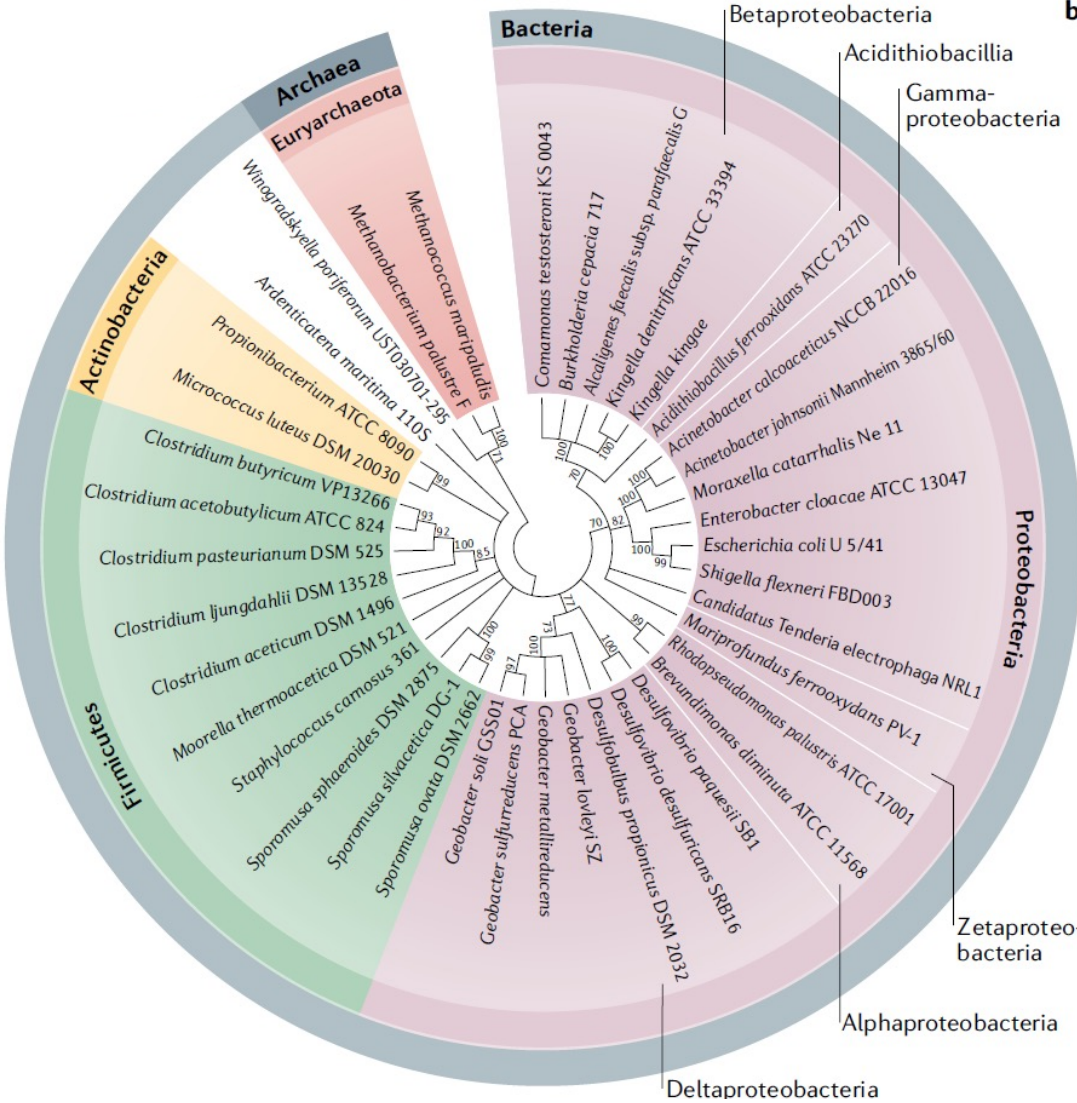
Exoelectrogenic microorganisms span all 3 domains of life!

- Bacteria
- Archaea
- Eukarya



Exoelectrotrophic microorganisms span 2 domains of life

- Bacteria
- Archaea
(no Eukarya)



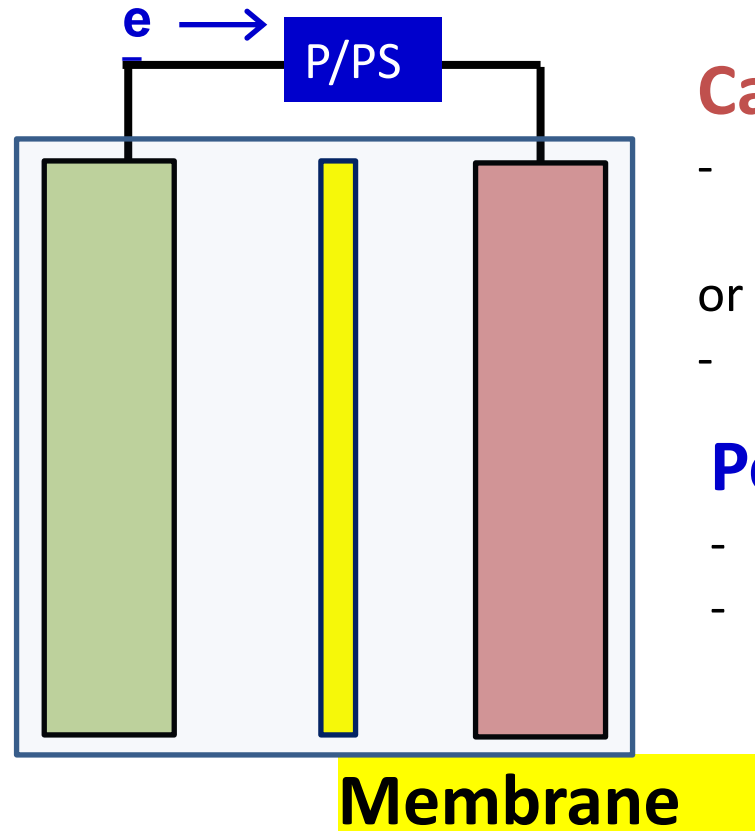
Bioelectrochemical Systems (BES)

BES: Any reactor with microbes and electrical current

MET: Microbial Electrochemical Technologies (MFC, MEC, etc.)

Anode

- Exoelectrogenic Microbes (Bioanode)
- or
- Abiotic (no microbes)



Cathode

- Electrotrophic Microbes (Biocathode)
- or
- Abiotic (no microbes)

Power

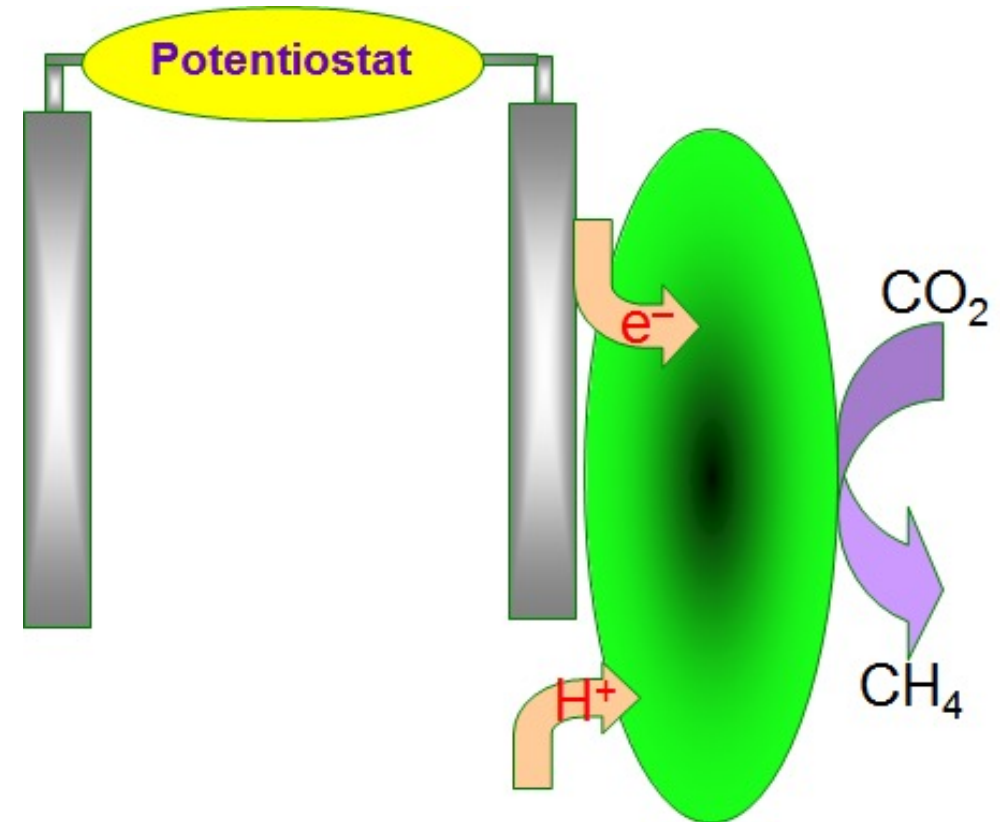
- Generated (P) = Microbial fuel cell (MFC)
- Added (PS) → Microbial electrolysis cells (MEC) for H₂ or CH₄ generation at the cathode

- None
- 1 or more

Many different chemicals can be used by electrotrophs to finally accept electrons from the cathode

Electron acceptors

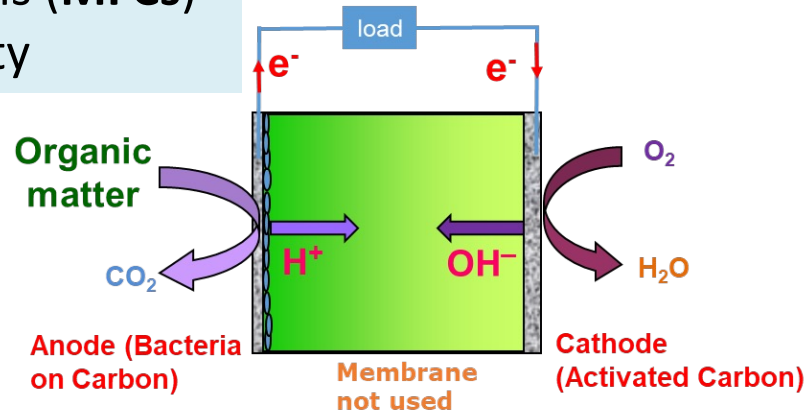
- Oxygen (makes electricity)
- Nitrate (denitrification)
- Metals (Copper plating)
- CO₂: reduction to produce organic compounds such as acetate
- CO₂: reduction by methanogens to make methane (CH₄)



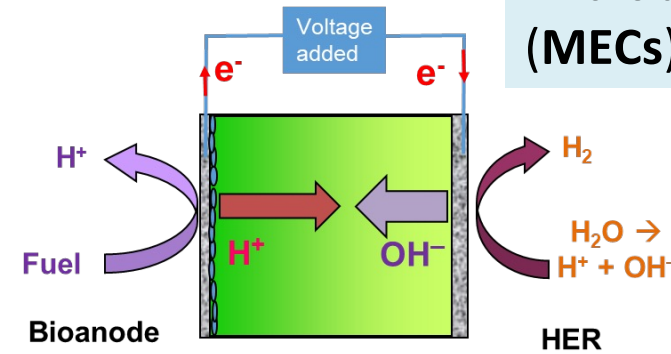
3 Main METs: MFCs, MECs, MMCs (MES)

Bacteria that generate electricity

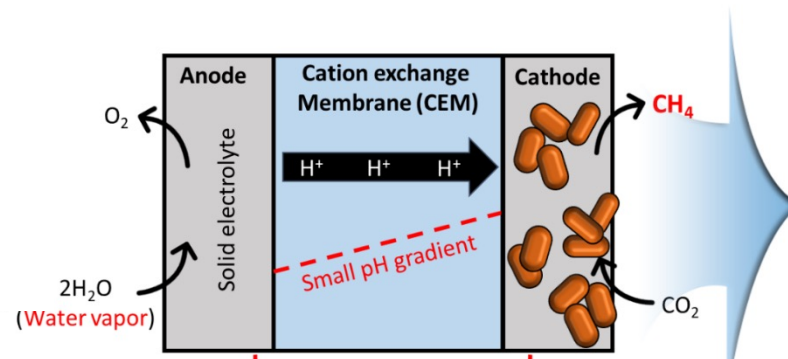
Microbial fuel cells (MFCs) produce electricity



Microbial electrolysis cells (MECs) produce H_2



Microorganisms that consume electricity (or H_2)



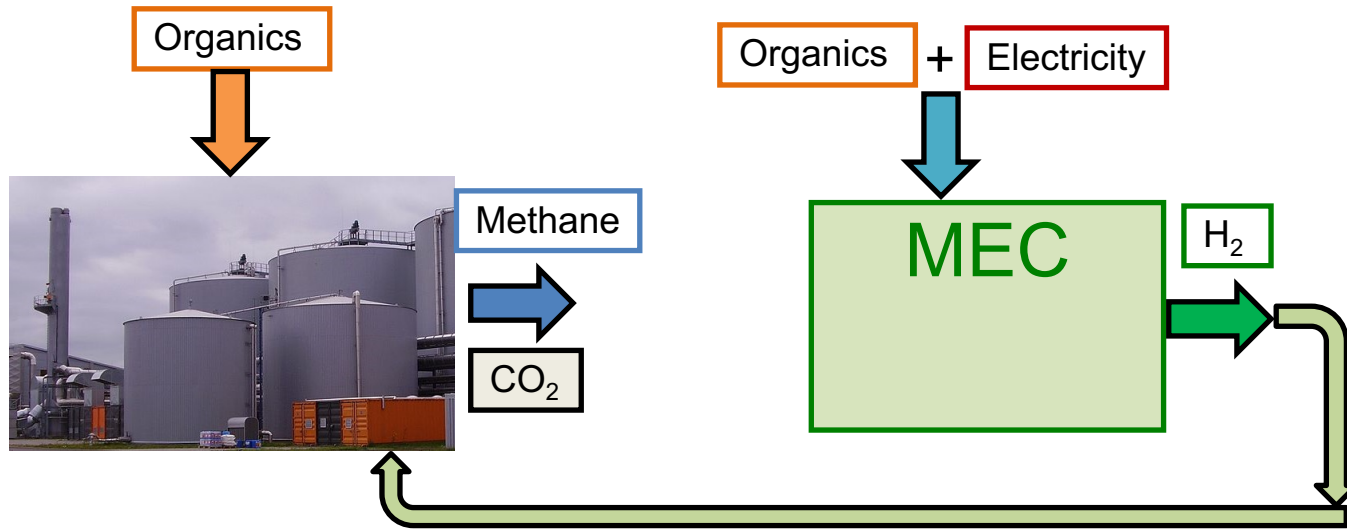
Microbial electrolysis cells (MES) produce chemicals

Microbial methanogenesis cells (MMCs) produce CH_4

MES: Microbial ElectroSynthesis of chemicals

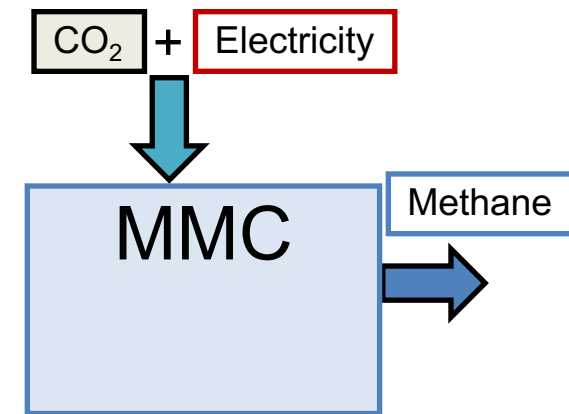
- BES → MES: Microbial electrosynthesis
- MET → MMC: microbial methanogenesis cells

AD= anaerobic digestion



MECs can make H₂

MMCs can make methane from renewable electricity

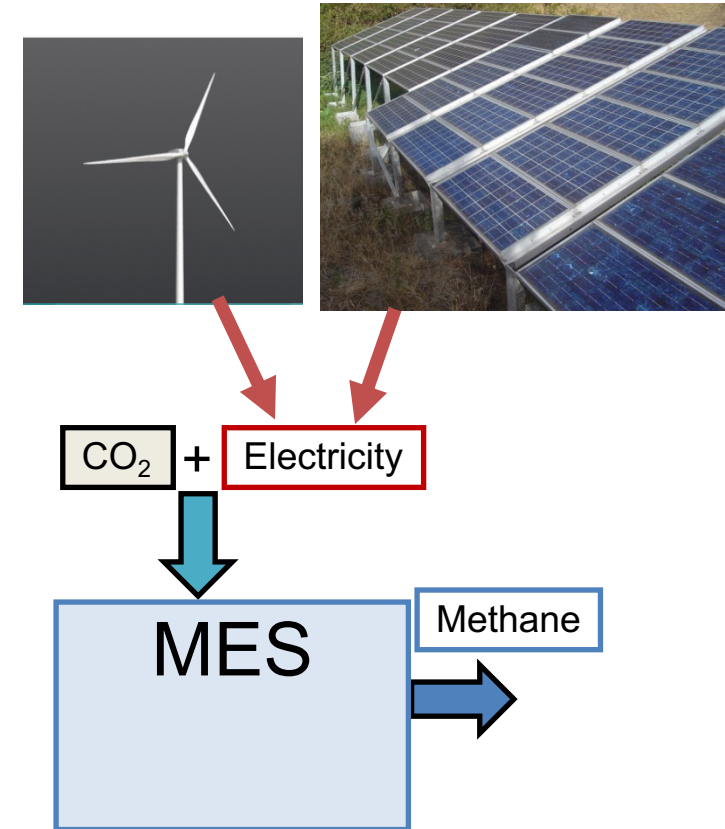


H₂ can be used to enhance methane concentrations and performance of anaerobic digesters (AD)

How can we move the MES technology forward?

1. Need to understand and optimize components
 - a. Most effective microorganisms?
 - b. How do methanogens get electrons?
 - c. What are the best cathode materials?
2. How do we construct the reactor?
 - a. MET: Different configurations
 - b. MMC: New designs for methane generation
 - c. Operation
 - d. Materials
3. What next?

- BES → MES: Electromethanogenesis
- MET → MMC: microbial methanogenesis cells

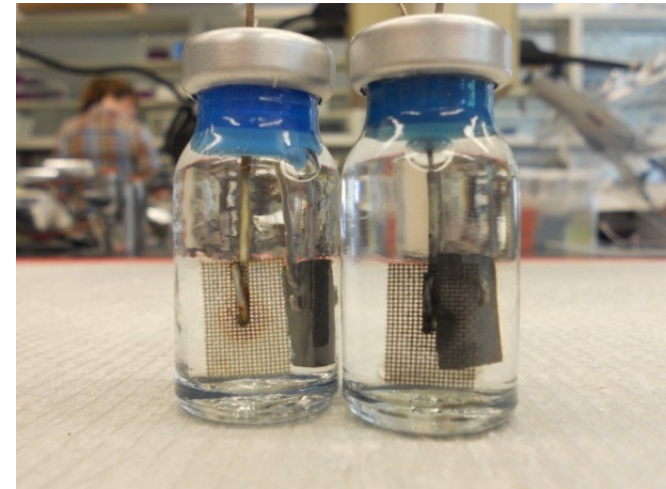


1a. What microbes are on the cathodes to make methane?

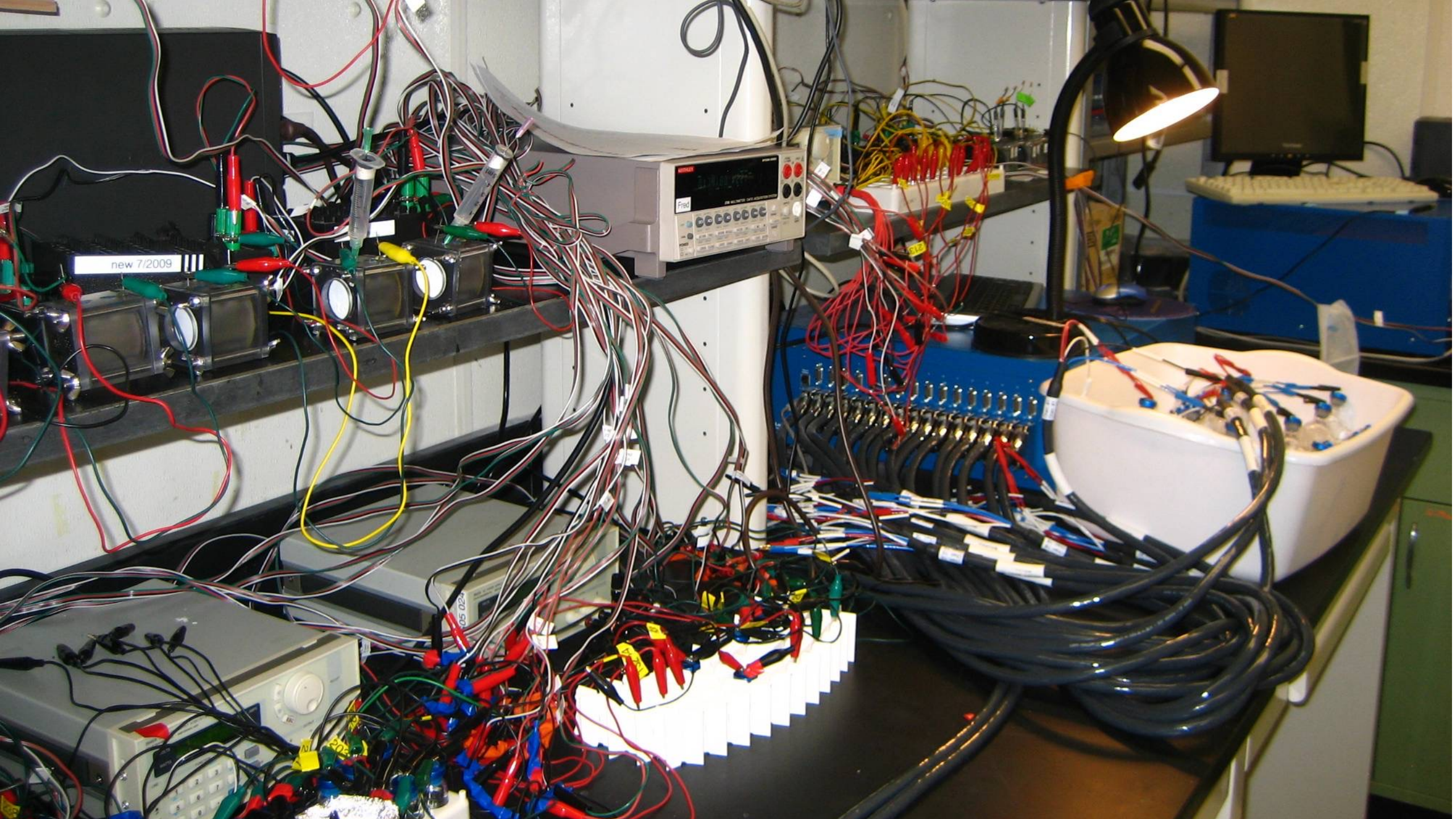
- Seek out diverse but rich sources of microorganisms
 - Anaerobic Digesters (AD), from the Penn State WWTP
 - Freshwater bog sediments (Bog)
- Examine in small reactors
 - Methane production with biotic anodes and cathodes
 - Amount of current
 - **Microbial community**

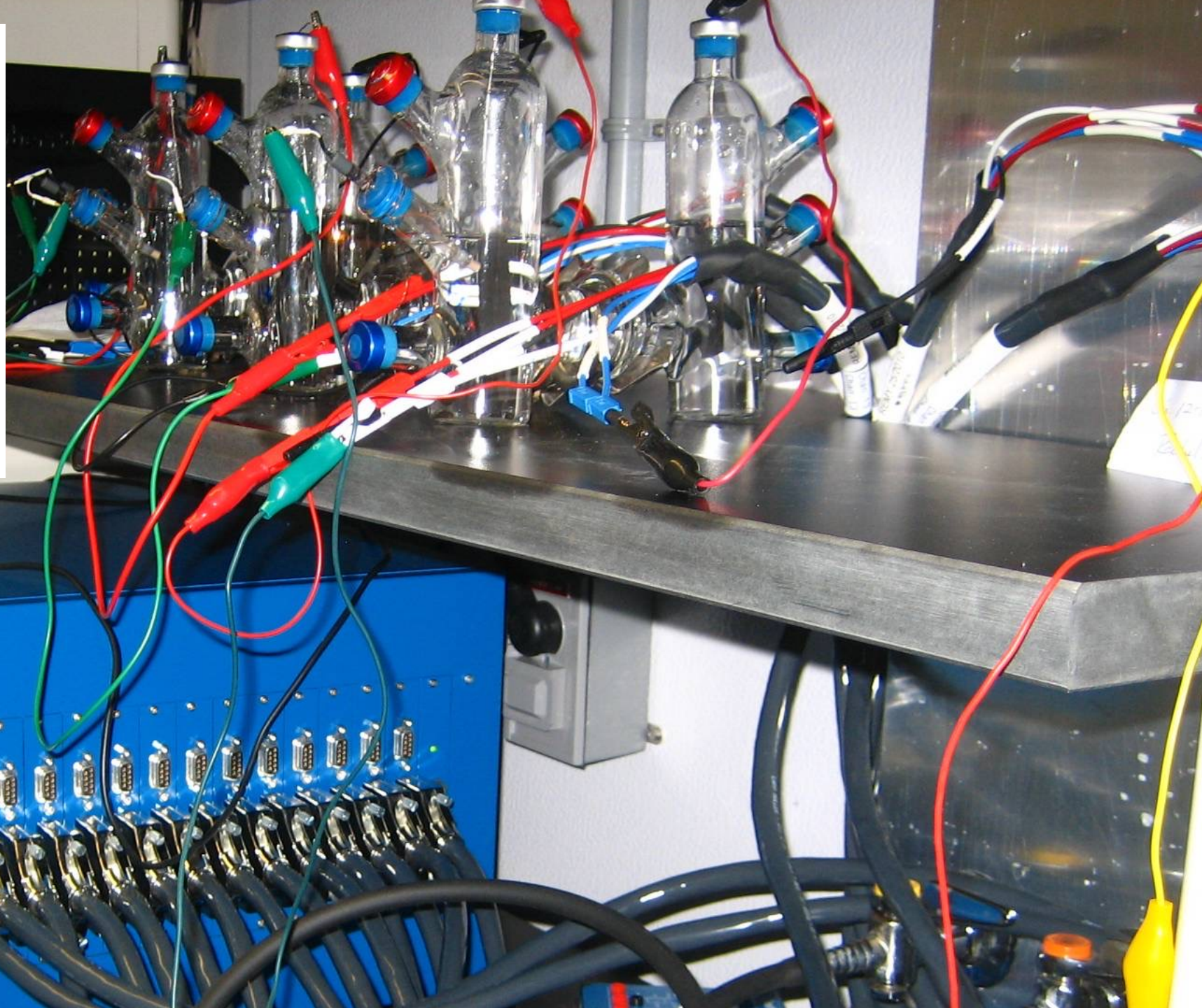
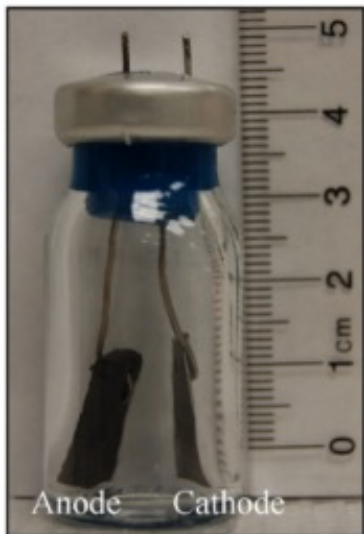


Call & Logan Biosens & Bioelectr 2011



Siebert, Li, Yates, Logan (2015) *Frontiers Microbiol.*

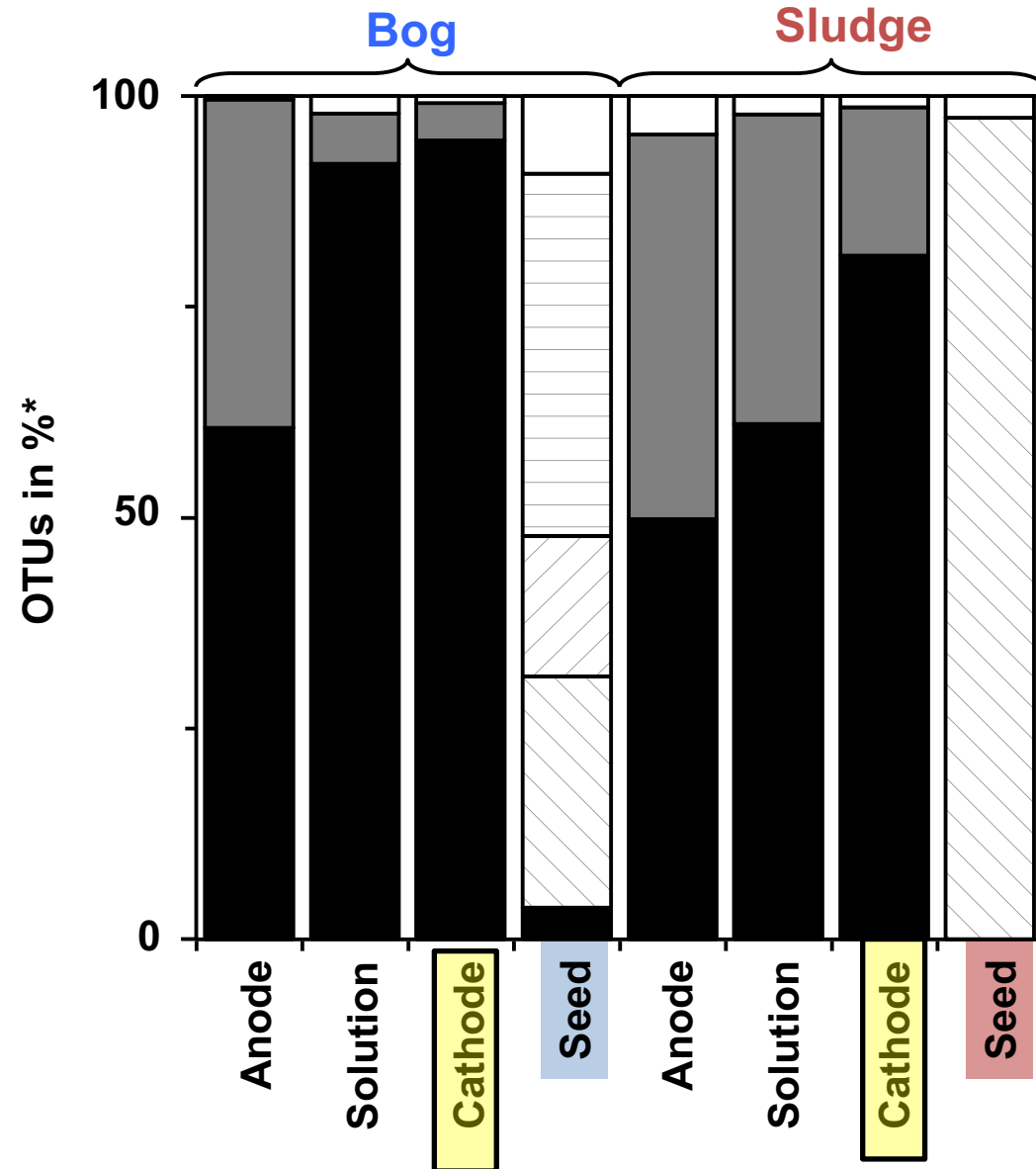




Cathode Communities (*Archaea*) are mostly *Methanobacterim*

- Others <10% each
- ▨ Miscellaneous Crenarchaeotic Gp
- ▩ Terrestrial Miscellaneous Gp
- ▧ *Methanosaeta*
- *Methanobrevibacter*
- ***Methanobacterium***

- Seed very different from final communities
- Final Bog and Sludge communities **similar** to each other
- Mostly *Methanobacterium*

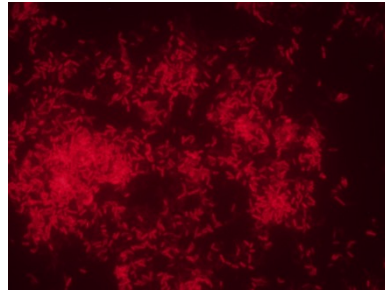


*OTU = operational taxonomic unit

Methanobacterium predominant (except with Pt)

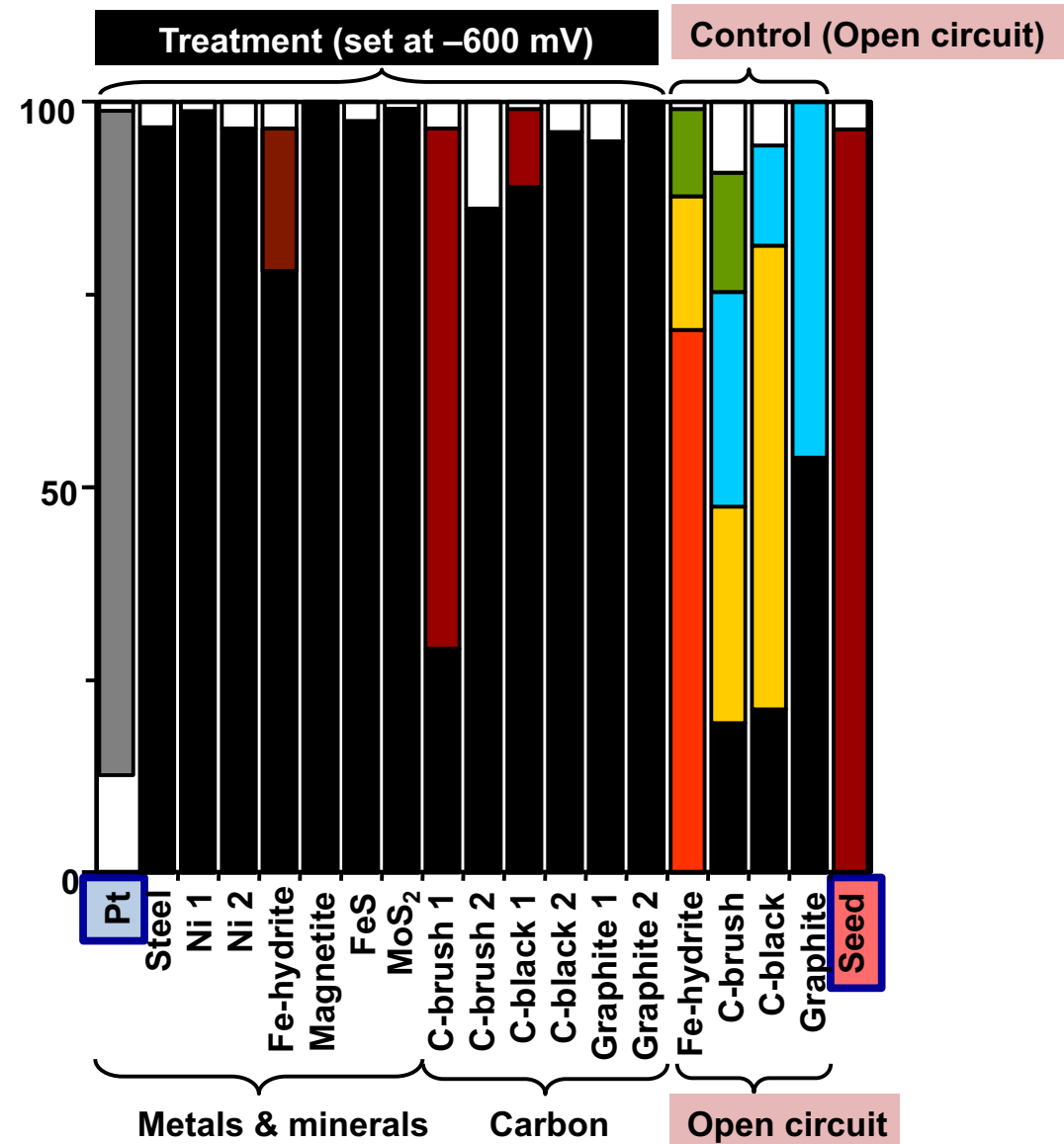


Methanobacterium : FISH probe



- Other *Euryarchaeota*
- Vadin CA 11 gut group
- TMG
- Methanomethylovorans*
- Methanosarcina*
- Methanosaeta*
- Methanobrevibacter*
- Methanobacterium***

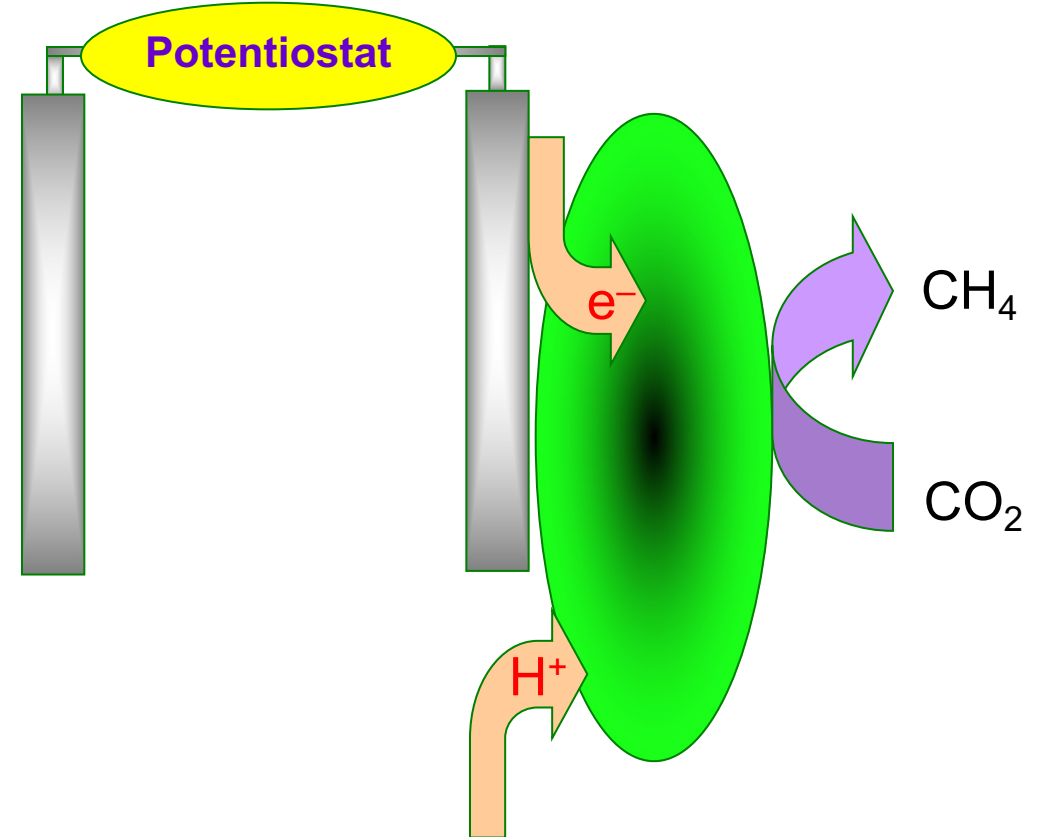
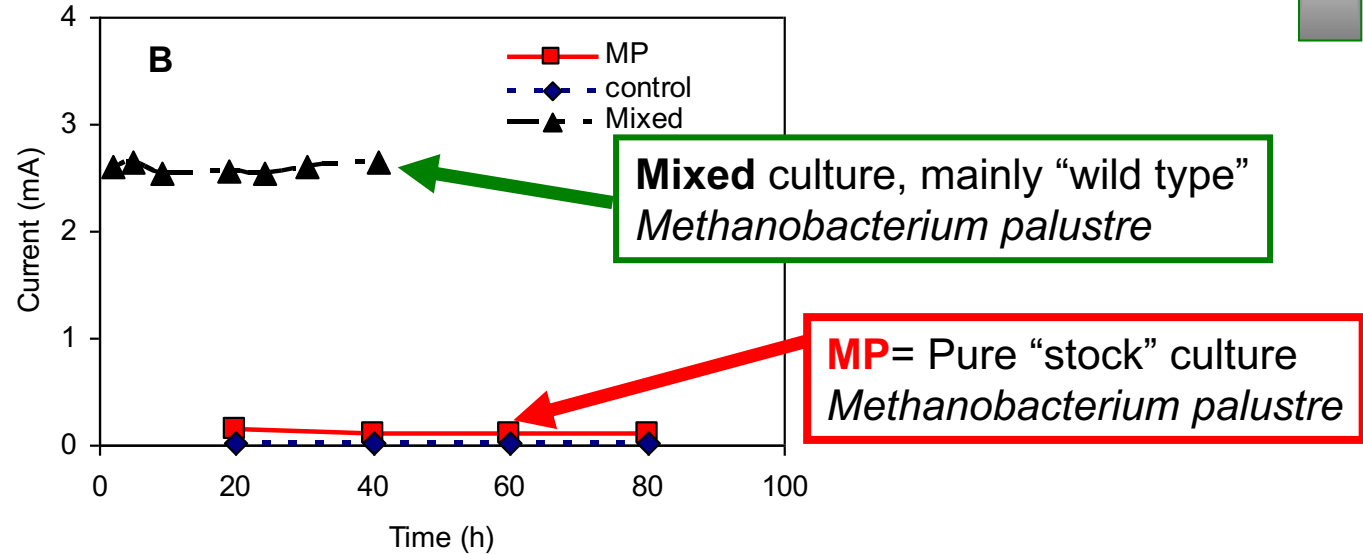
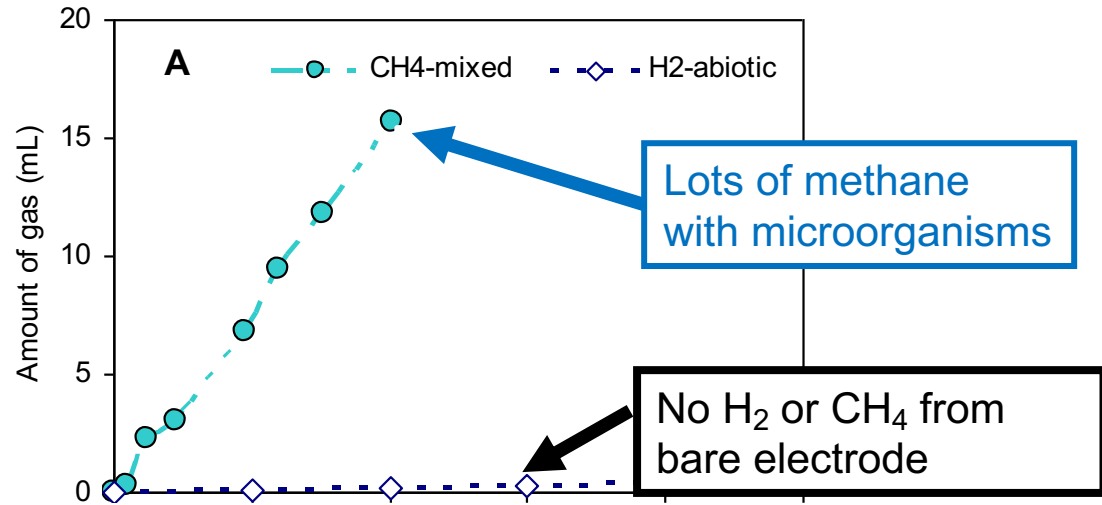
OTUs in %*



*OTU = operational taxonomic unit

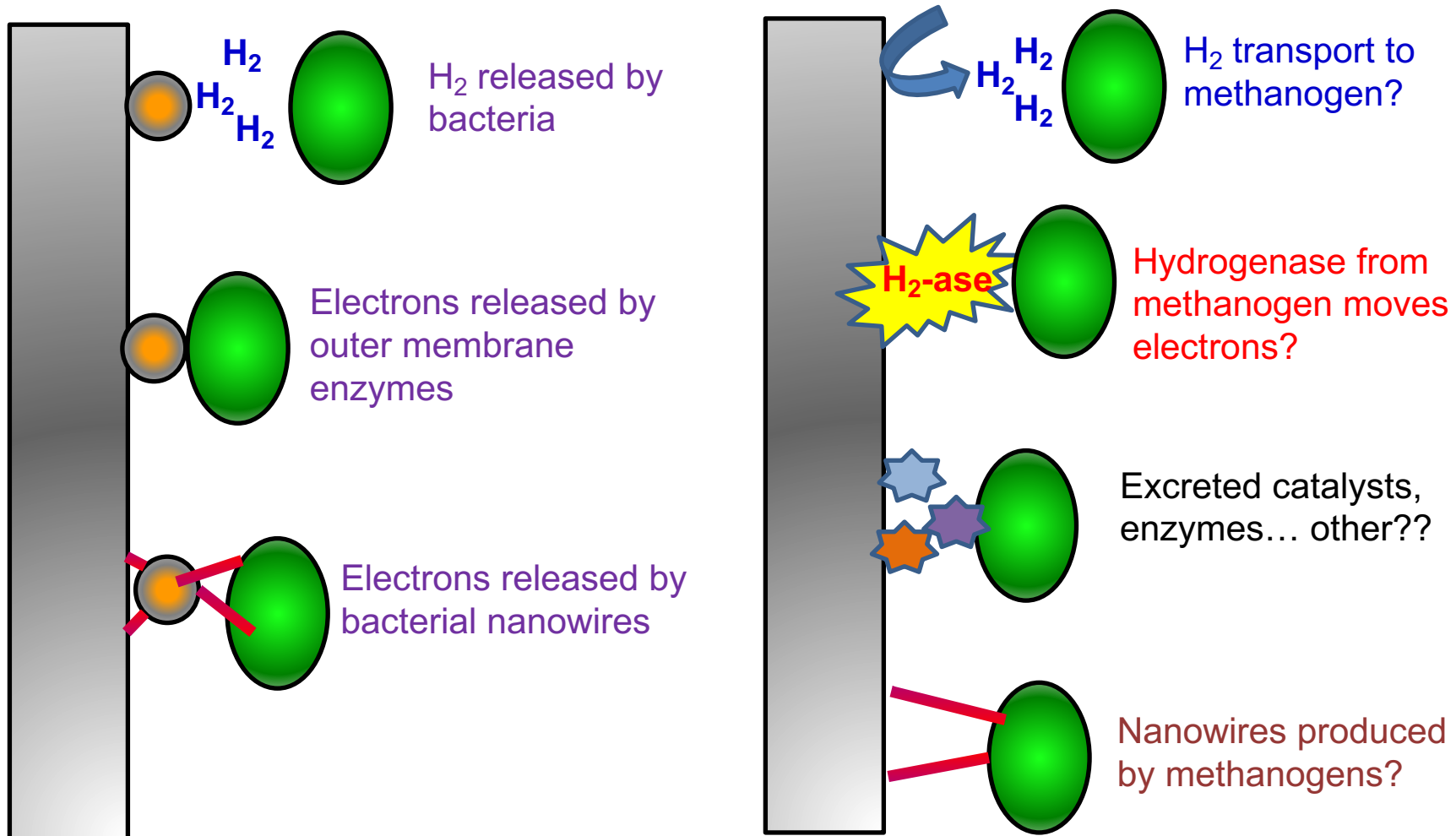
Siegert, Yates, Spormann, Logan (2015) *ACS Sus. Chem. Engin.*

Electrotrophic Methanogens: facilitate current



1b. How do electrons get to methanogens?

Key:  Bacterium  Methanogen



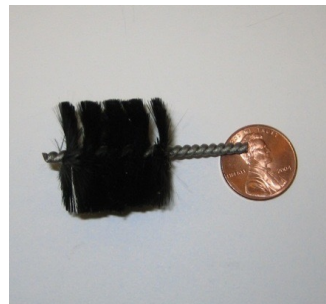
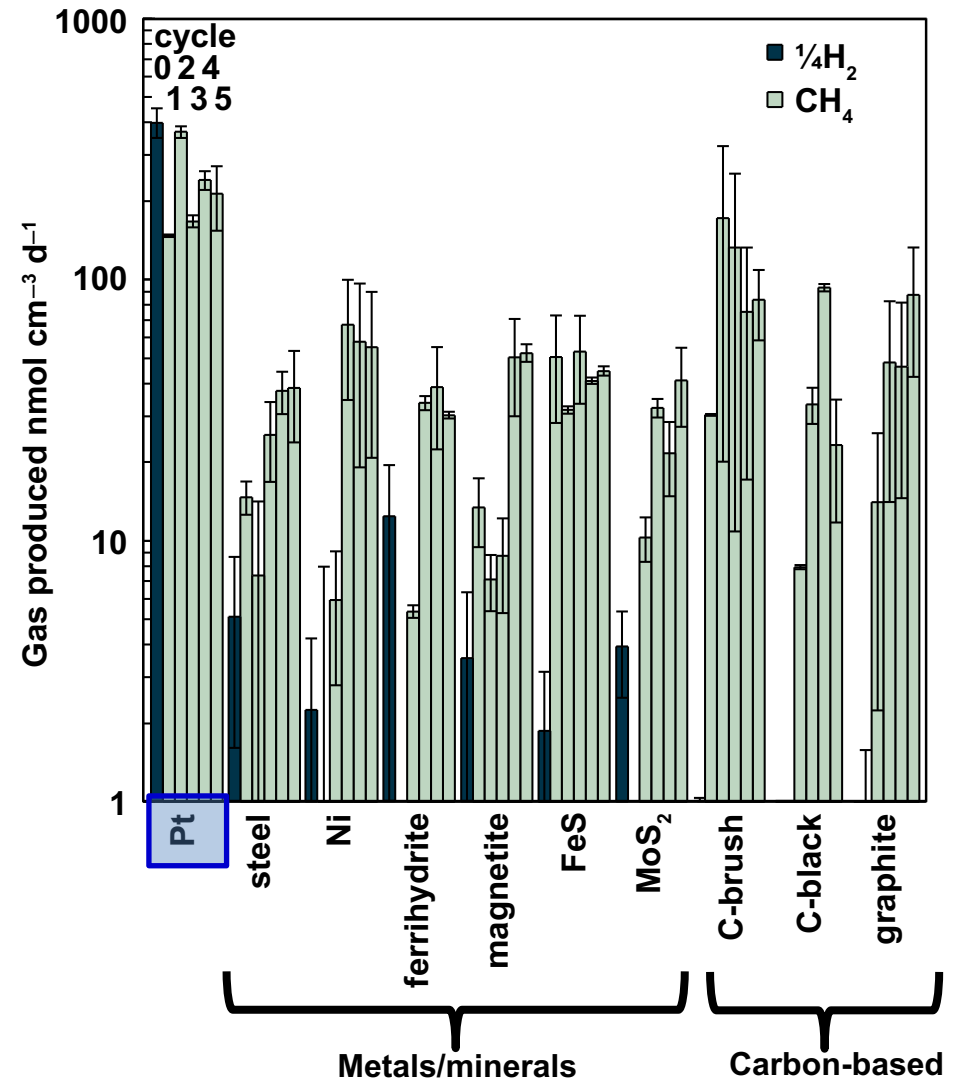
1c. Best cathode materials for methane production in MMCs?

- **Materials can affect MES through changing:**
 - H₂ evolution rates: Adding catalysts impacts how fast H₂ can be released from the surface
 - How methanogens take in electrons or their enzymes interact with the surface
- **Materials Tested:**
 - **Platinum:** the best catalyst for H₂ evolution
 - Metals & Minerals that are good catalysts and inexpensive: **Stainless Steel, Ni, MoS₂; ferrihydrite, magnetite, FeS**
 - Carbon: not good catalyst, very cheap: **carbon fiber brushes** have very high surface area!



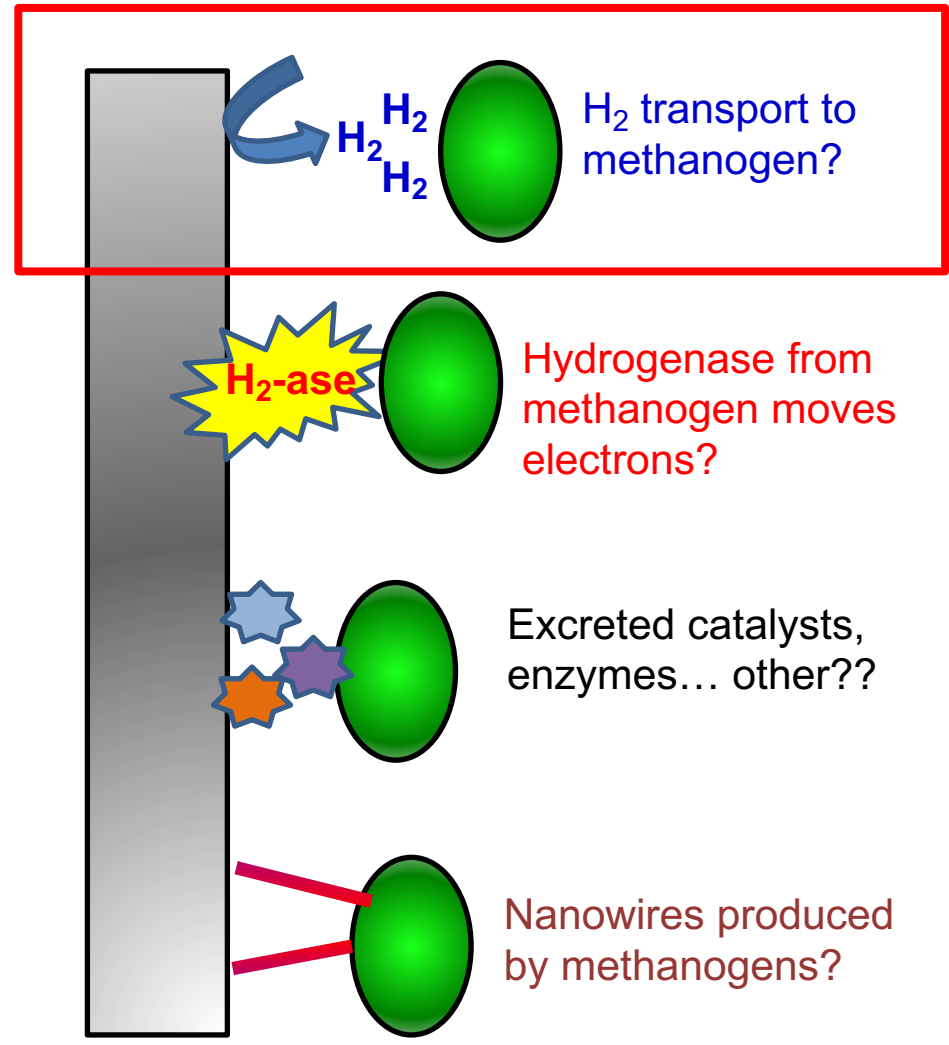
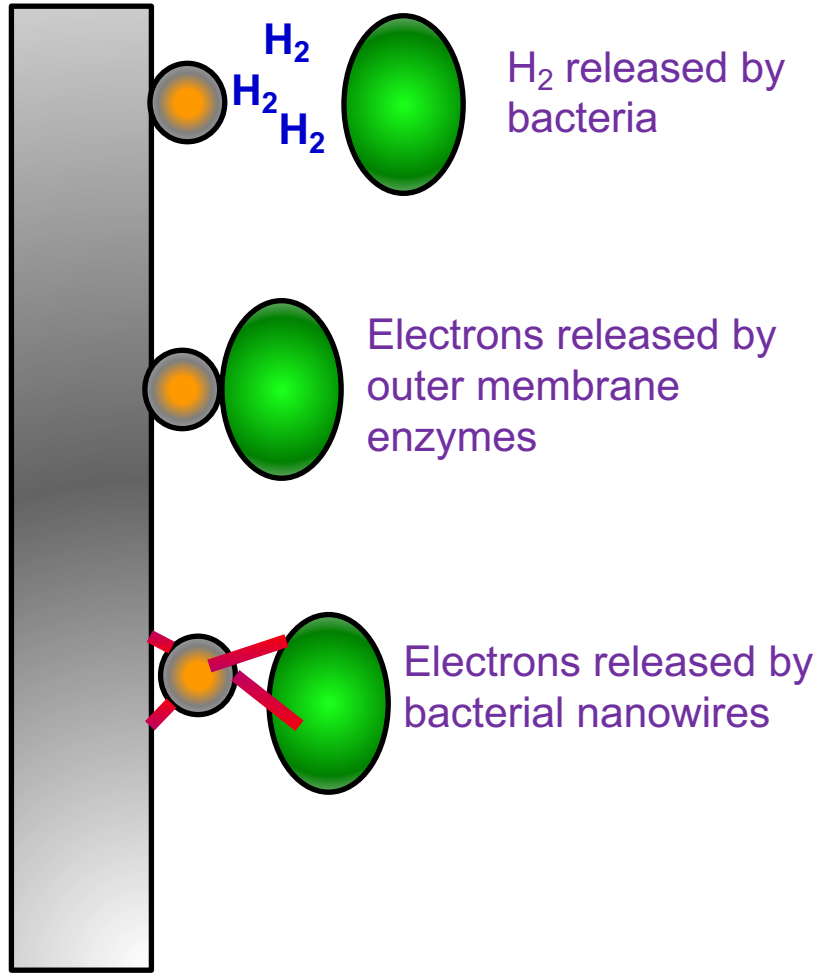
Effect of cathode materials on CH₄ production

- If current forms H₂, that is the blue bar
 - 4 moles hydrogen needed to form 1 mole of methane
- Platinum (Pt) is the best
 - Noble metal, expensive
 - Agreement of blue and green bars indicates H₂ gas produced that was then used to make methane
- Carbon brushes
 - Next best material
 - High surface area of carbon brushes likely facilitates direct electron transfer



Key:  Bacterium  Methanogen

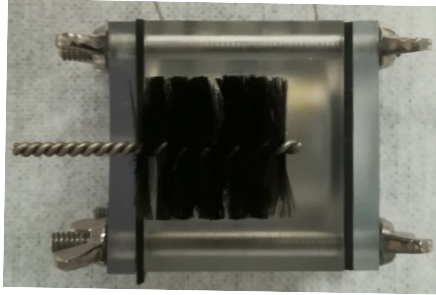
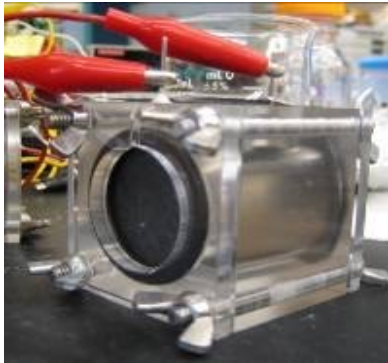
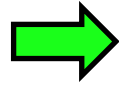
Using H₂ likely most important for high rates



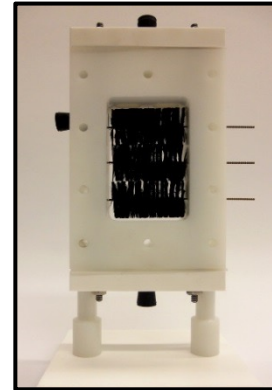
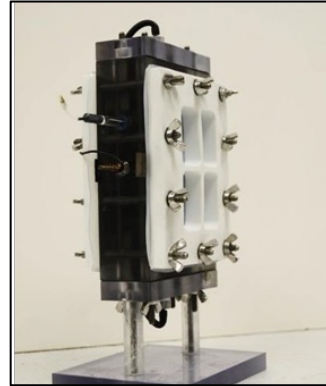
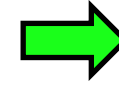
2a. Scaling up METs:

2a. Scaling up METs: Pilot-scale MFCs for electricity

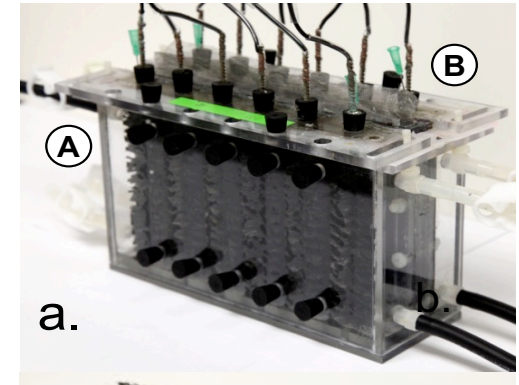
Gen 0: 0.025 L, $25 \text{ m}^2/\text{m}^3$



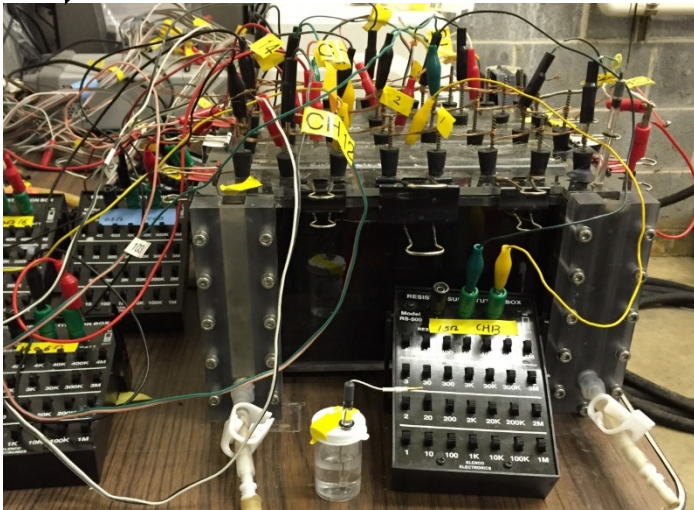
Gen 1: 0.13 L, $25 \text{ m}^2/\text{m}^3$



Gen 2: 2 L, $20 \text{ m}^2/\text{m}^3$



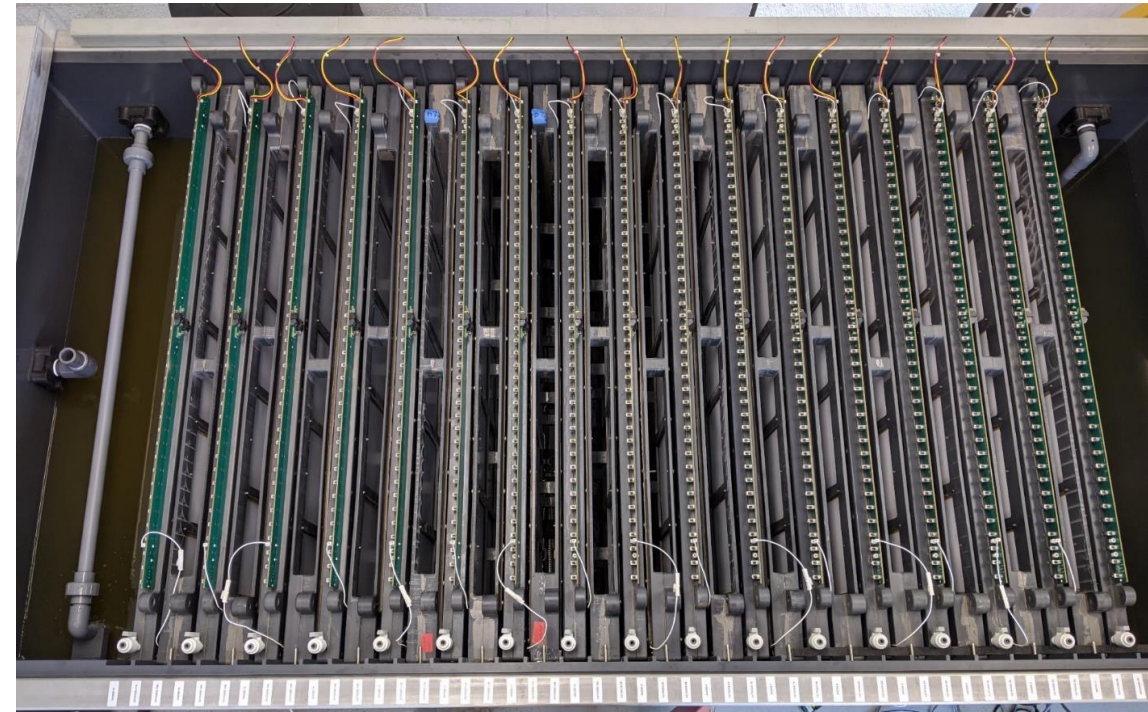
Gen 3: 6.1 L, $20 \text{ m}^2/\text{m}^3$



Pilot-Scale MFC:
850 L active
volume, $25 \text{ m}^2/\text{m}^3$

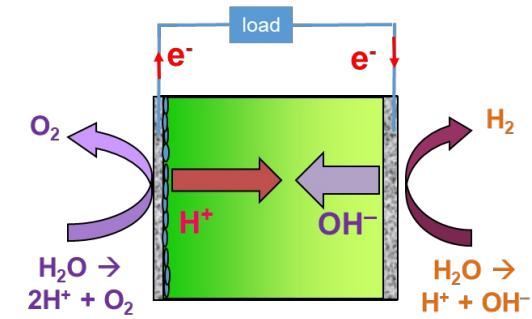


CONSTRUCTIVE
ENGINEERING
RESEARCH
LABORATORY



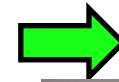
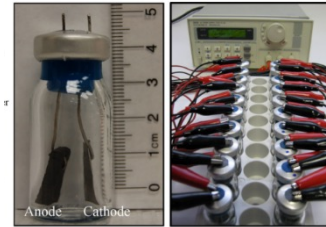
PennState

Scaling up MECs for H₂ gas: from 5 mL to 1000 L

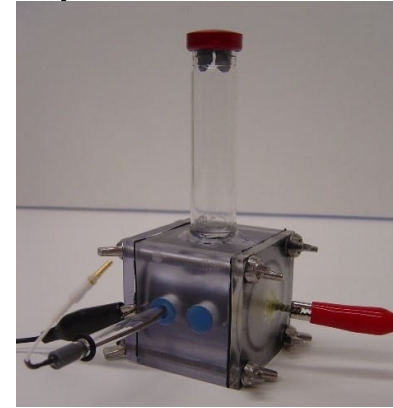


Single-Chamber MECs: H₂ → CH₄
 Thus, methane not H₂ is the product gas

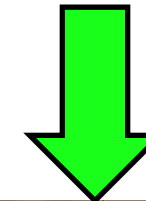
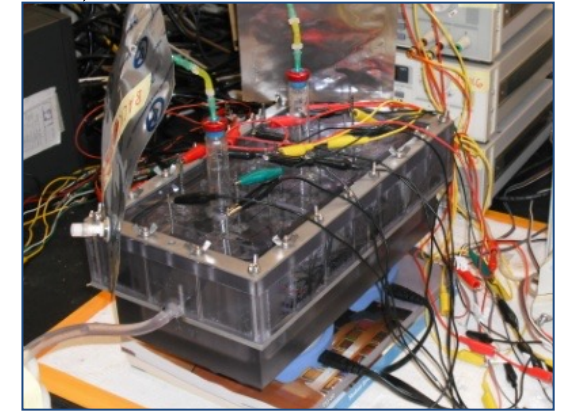
5 mL mini-MEC



28 mL MEC




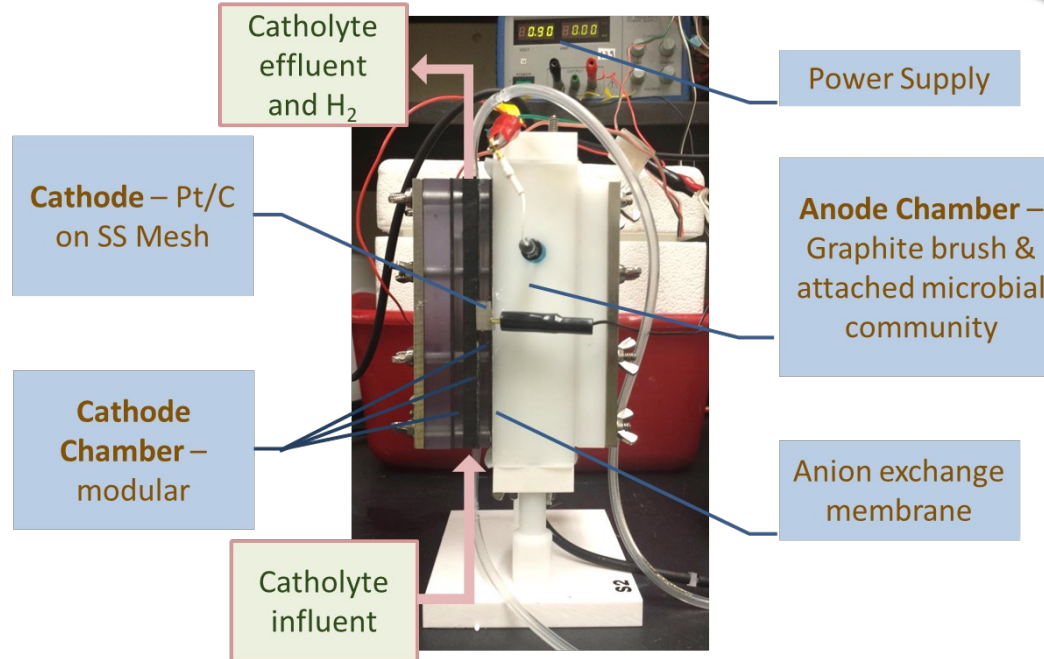
2.5 L MEC



1000 L MEC




Two-Chamber MECs are needed for H₂ recovery



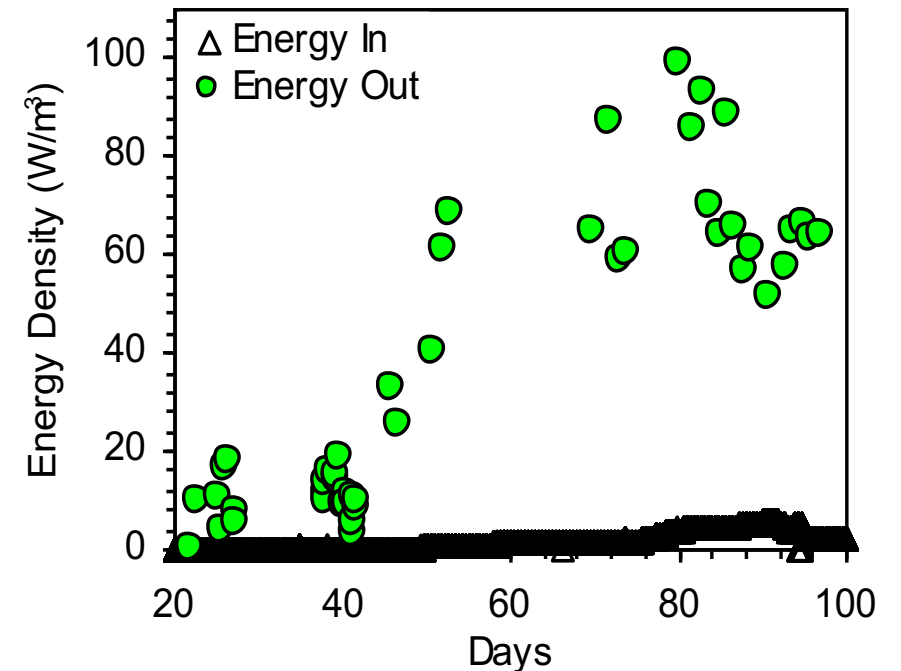
MECs can produce methane from organic matter in dilute wastewaters



CH_4 was produced from wastewater with small energy input

- Elec. Energy in = 6 W/m^3
- Energy Out (CH_4) = 99 W/m^3

16× more energy recovered than electrical energy put into the process



2c. Scaling up MES: Methane Generation from Water Splitting

1 Chamber: Generate O_2 at the anode



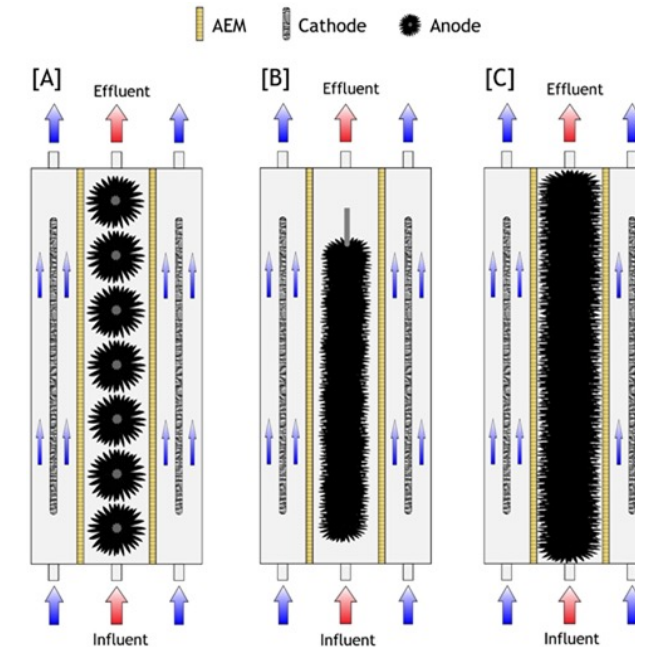
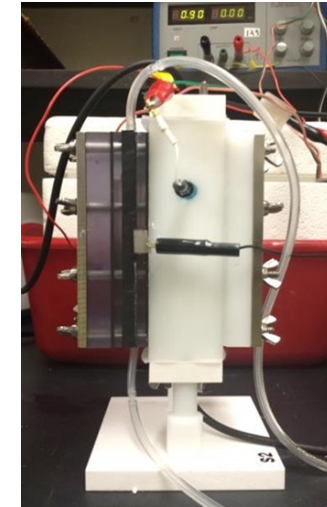
2 Chamber Bottle reactors: not suitable for scaling up



2 C: keeps O_2 in separate chamber

Challenge 1 C system: O_2 kills methanogens

2 Chamber Brush electrodes: Need too much space (need compact reactors)



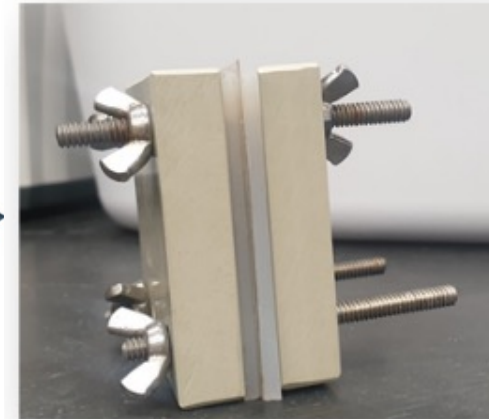
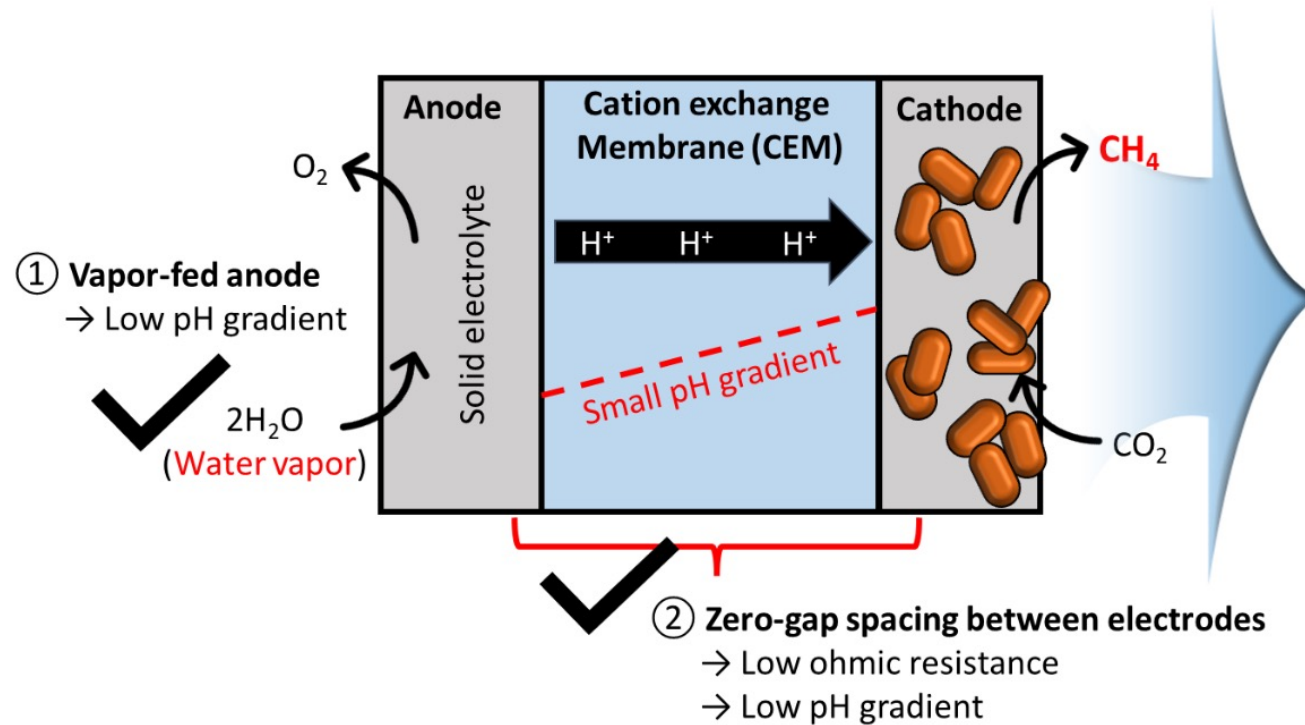
The Challenges of these 2 C systems

- Wide (or separate) chambers = large energy losses
- The electrode with methanogens gets a high pH

Compact MMC for water splitting & biocathodes

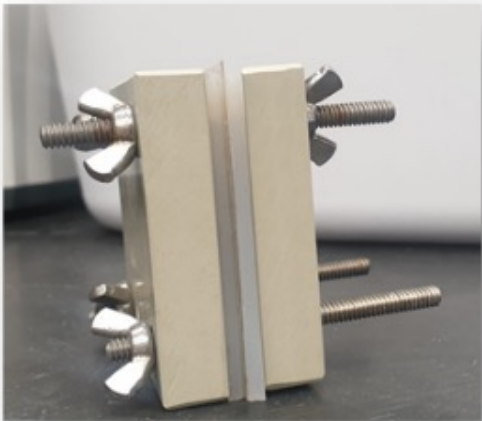
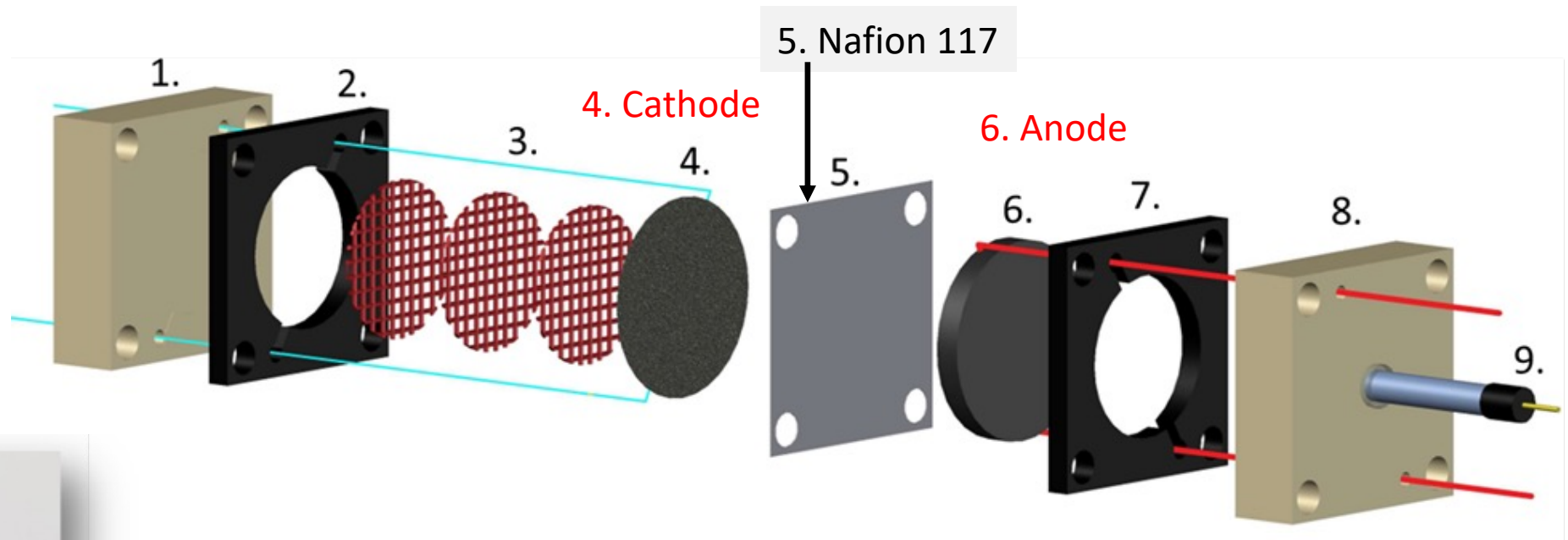
The process

- **Anode:** H^+ produced with O_2 generated by water splitting anode (electrochemical)
- **Membrane:** CEM (cation exchange membrane) transports only H^+ to cathode
- **Cathode:** H^+ combines with OH^- released from anode
- **Methane** is biologically produced by methanogens on the cathode



Reactor is very compact!

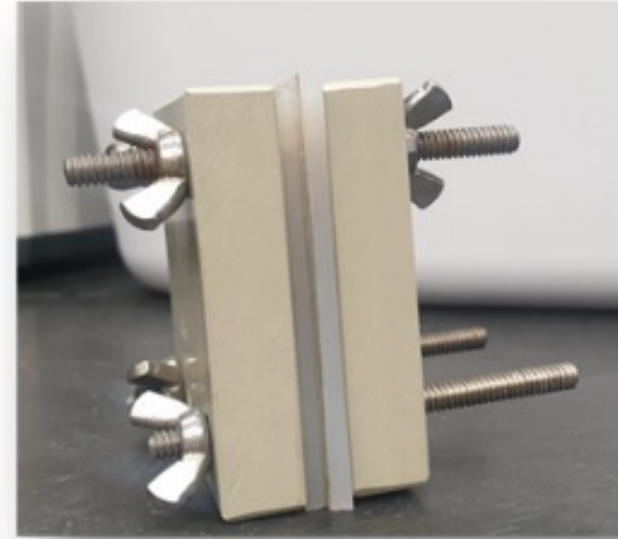
Water-splitting MMCs have not been scaled up ...



There can be many of these cell pairs in a stack.
Just one cell pair shown here

2d. What have we achieved in MMCs?

- New compact (slab) systems
 - Most energy efficient MMC ever designed: ohmic resistance was $2.4 \pm 0.5 \text{ m}\Omega \text{ m}^2$
 - Improved gas production: 2.9 L/L-d (17 A/m^2)
- Previous (bottle) systems
 - Very energy intensive due to high ohmic resistance: $20\text{-}25 \text{ m}\Omega \text{ m}^2$ ($10\times$ higher)
 - $1000\times$ lower gas production (0.0062 L/L-d)



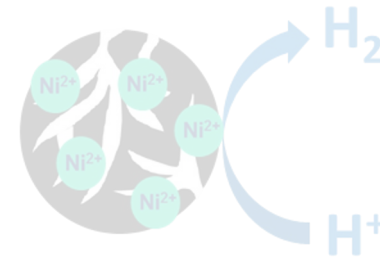
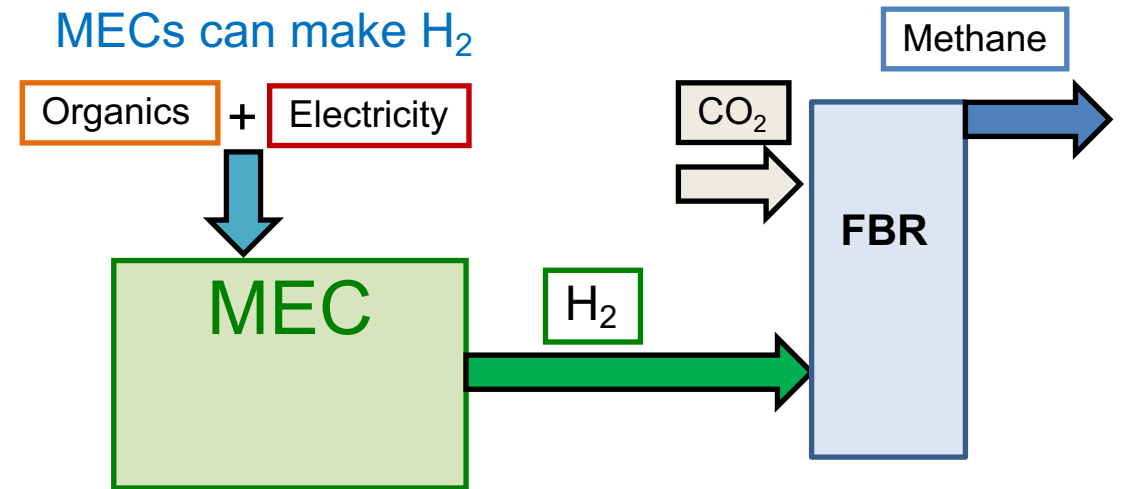
Costs to produce CH₄: Only electricity

| Conditions | Euro | Danish krone |
|---------------------------------|----------------------|----------------------|
| Electricity cost | 0.35 €/kWh | 2.6 kr/kWh |
| Natural gas cost (home)- volume | 2.3 €/m ³ | 17 kr/m ³ |
| - energy | 0.19 €/kWh | 1.4 kr/kWh |
| Renewable biomethane – volume | 2.5 €/m ³ | 19 kr/m ³ |
| - energy | 0.23 €/kWh | 1.7 kr/kWh |

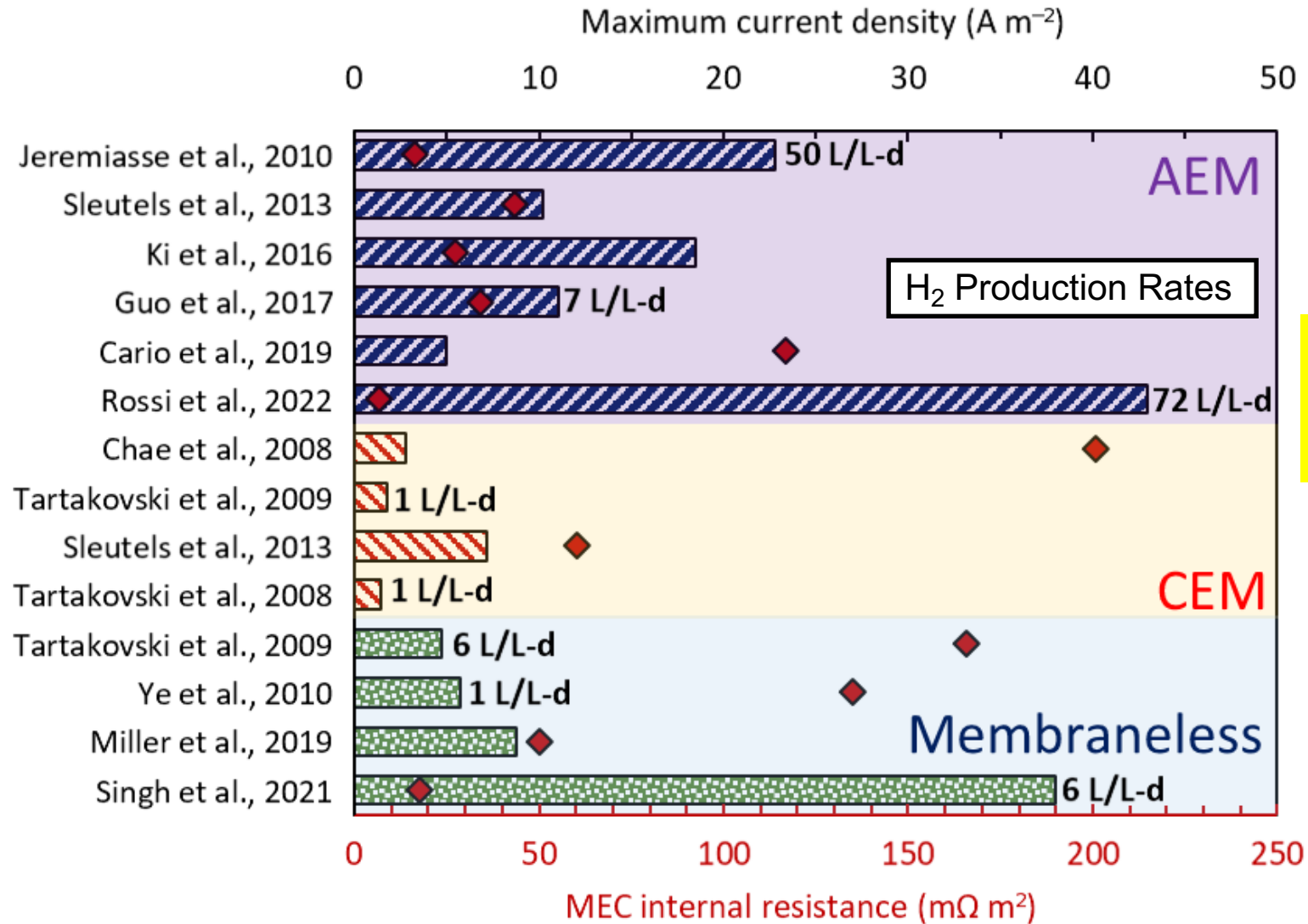
- Energy in 1 m³ of natural gas = 12.2 kWh
 - Same energy in 1.3 L of petrol
 - More energy needed than energy in the gas (thermodynamics)
- Efficiency of changing electricity → CH₄?
 - Currently 17% → This can be improved!
- For comparison: reverse process of CH₄ → electricity
 - Currently 33-65% efficiency based on energy

2e. Future Directions in Electrosynthesis of Methane

- Generate Hydrogen first?
 - Use and MEC? But that requires a source of organic matter for the anode.
 - Rates of MEC > MMC
- Cheap, efficient cathode catalysts
 - Brush and carbon electrodes lack a cathode catalyst.
 - Could we use non-precious metal Ni-based catalysts developed for MECs in MMCs?



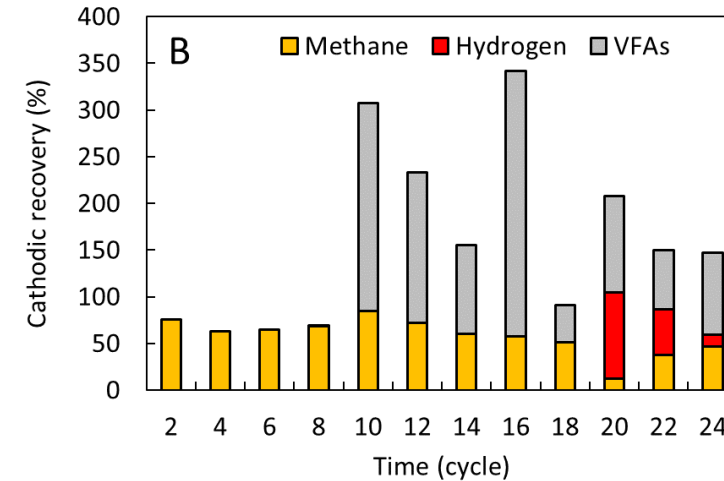
H₂ production rates by MECs are higher than CH₄ in MMC



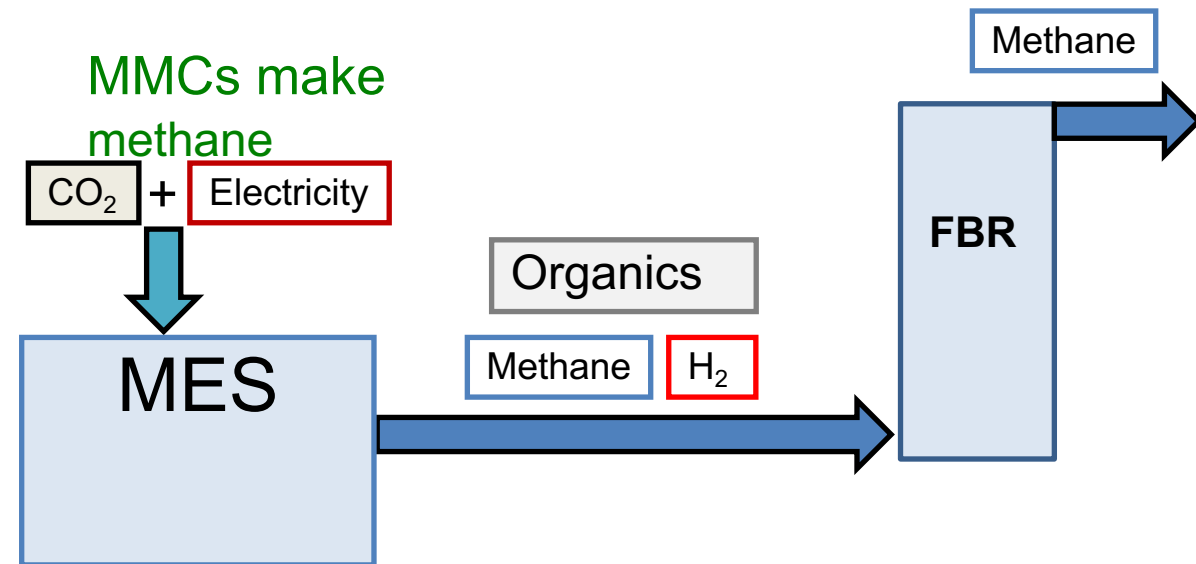
72 L/L-d H₂ =
18 L/L-d CH₄

Other chemicals can be produced in MES

- MMC indicates methane is primary product, but MES = other products
- Using mixed cultures (many microbes) and applying a high voltage can also release
 - H₂ abiotically from the cathode
 - Organics or “VFAs” (acetate, formate, etc.) appear in later cycles at higher applied voltages
- Adding a fluidized bed bioreactor (FBR) could further convert these to more methane
 - Advantage is higher current density, so more methane per MES reactor

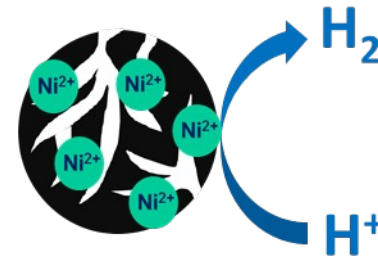
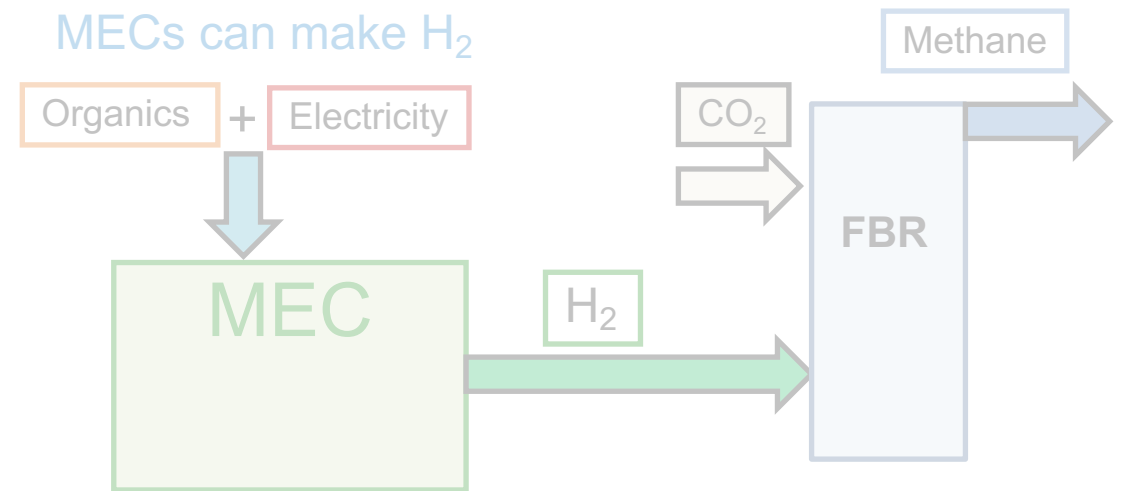


Can also produce H₂ and organics (VFAs)



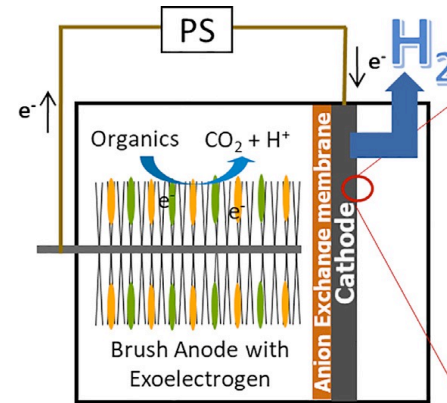
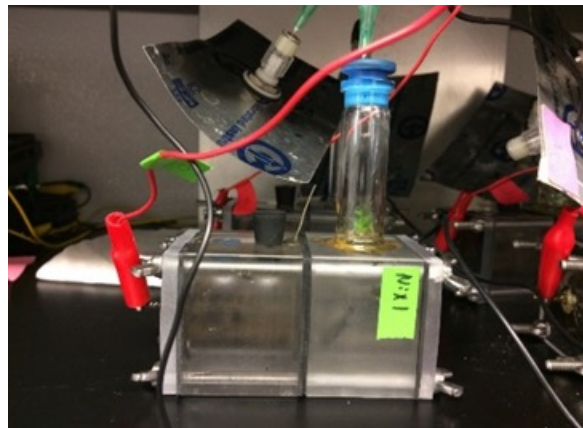
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 - Could we use non-precious metal Ni-based catalysts developed for MECs in MMCs?



What are suitable materials and catalysts for MMCs?

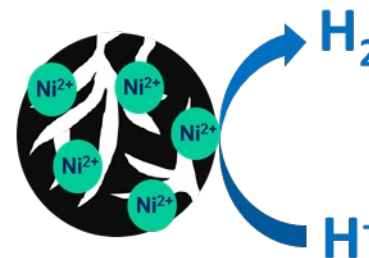
- Need inexpensive catalysts
 - Carbon electrodes is not good catalysts.
- Materials previously tested
 - Non-precious metals like **stainless steel (SS)** or Ni-based catalysts such as **Ni** particles and **Ni₂P** used
- Better materials being developed



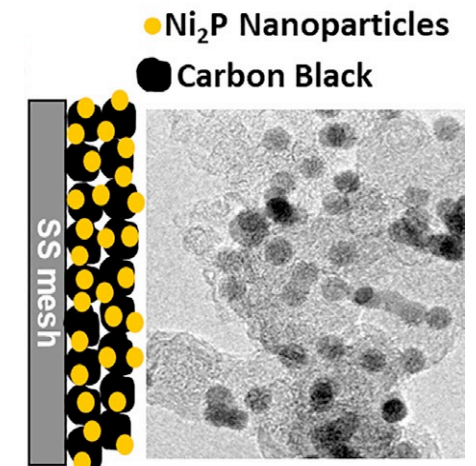
Stainless Steel wool cathodes



Nickel particles, pNi on activated carbon



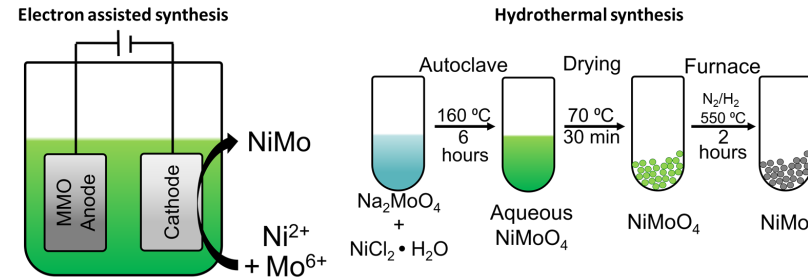
Nickel Phosphide Ni₂P



New, more effective Pt Catalyst: NiMo

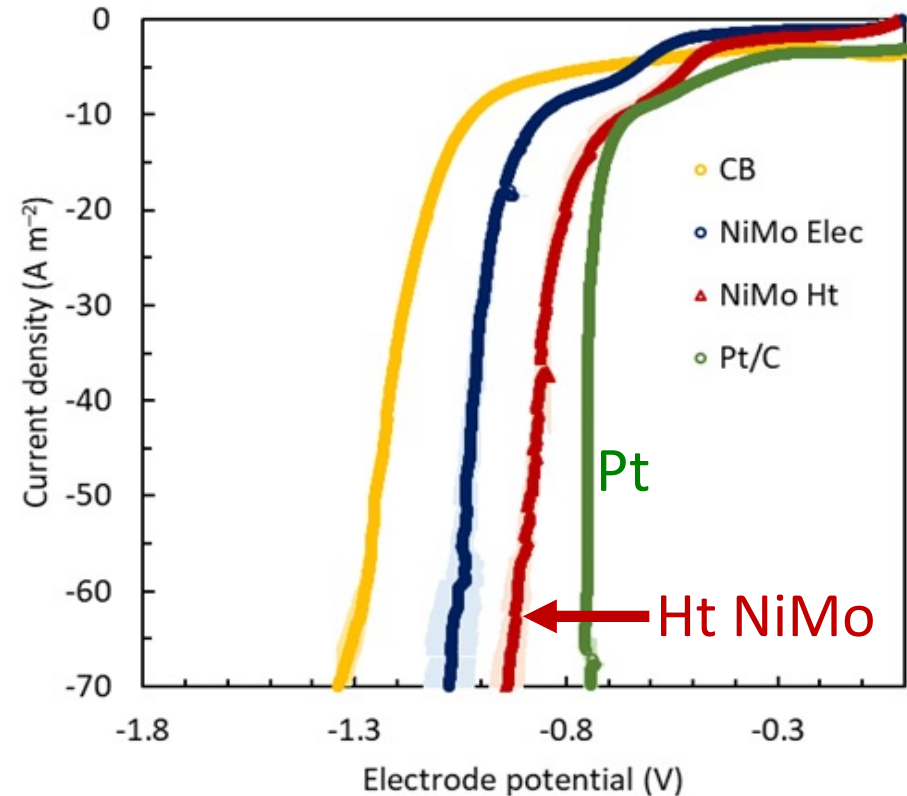
- **Method 1: Hydrothermal method (Ht) (shown on right)**

- Many steps
- High energy use



- **Method 2: Electrochemical method (Elec)**

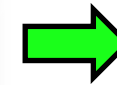
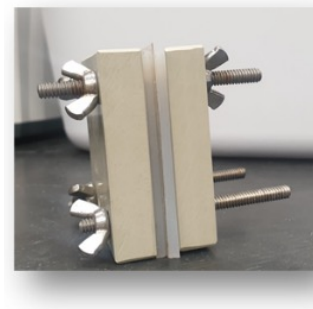
- Simple procedure: Electrochemical deposition of catalyst is very desirable
- Well controlled conditions
- But... lower performance than Ht method (so far)



3. Scaling Up Compact Reactors

- **MFCs** and **MECs** have reached 1000 Liter scale
- Engineering 1000 L **MMC** will be a fun engineering challenge!
- Stay tuned...!

What will the MMC look like?



Active area = 7 cm^2
(1 electrode)

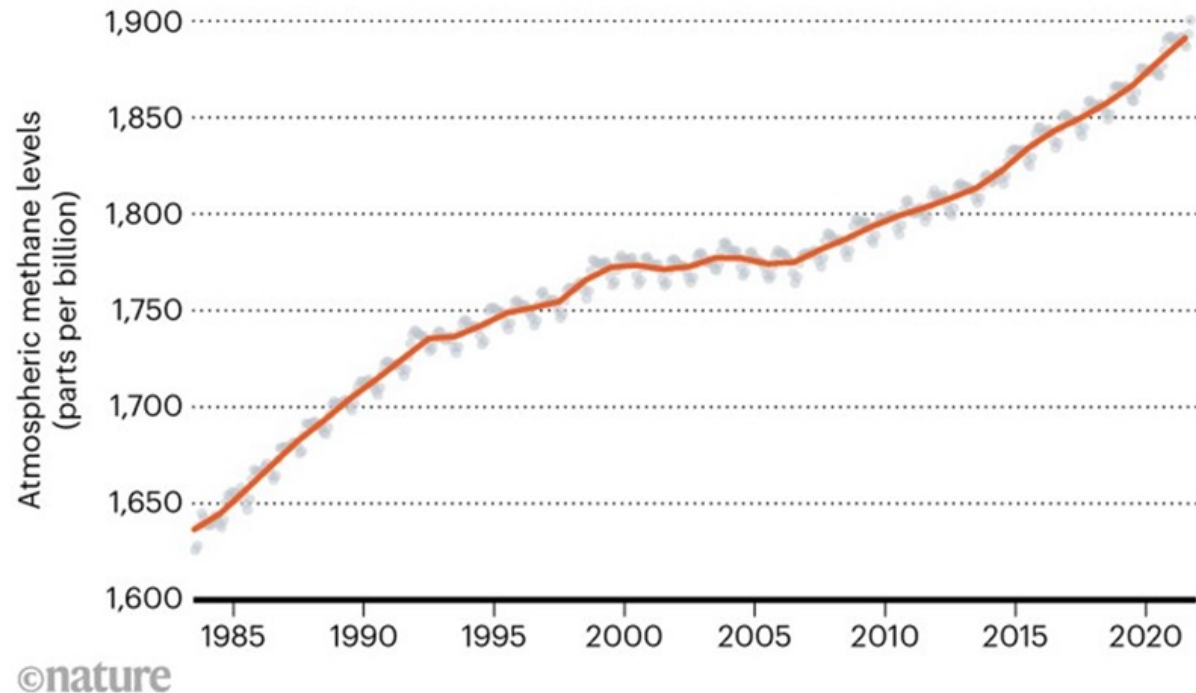
Active area = 0.42 m^2
(4200 cm^2) x 6 electrodes

Final Note: Avoid Methane Emissions!

- Methane is a potent greenhouse gas, with a global warming potential (GWP) of:
 - 25× CO₂ over 100 yr
 - 85× CO₂ over 20 yr (more appropriate)
- Almost no difference in atmospheric impact from fossil or renewable CH₄
- Redefining the GWP of methane (from 25 to 85) increases GHG emissions by 25% in the USA

A WORRYING TREND

Atmospheric methane levels have been rising since the Industrial Revolution. Growth slowed between 1999 and 2006, but methane levels have increased sharply since 2007. Neither trend is well understood.



CONCLUSIONS: Green Methane Makes Sense!

- Advances in MET designs have made it possible to develop thin and energy-efficient reactors for CH₄ and H₂ production.
- Achieved 3 L/L-d of CH₄ in preliminary (non-optimized) tests.
- Should be able to substantially increase CH₄ production rates due to 89 L/L-d of H₂, equivalent to 18 L/L-d of CH₄.

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U.S. DEPARTMENT OF
ENERGY



PennState



Special acknowledgements to:

Dr. Ruggero Rossi
Asst. Research Prof.
(Penn State → Johns Hopkins Univ.)
Pioneering work on zero-gap MFCs and MECs.



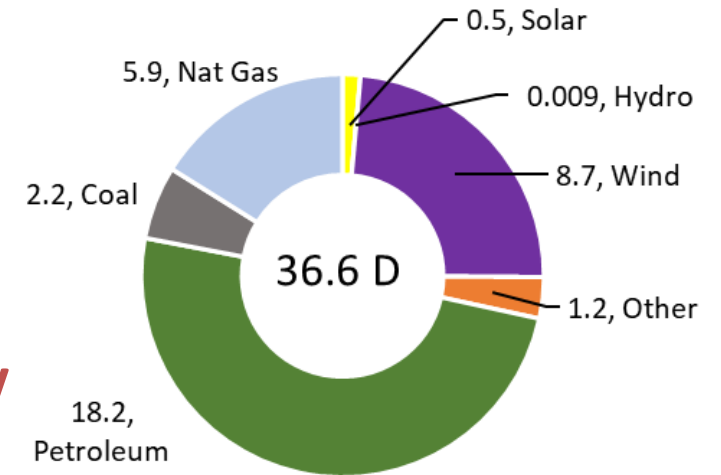
Dr. Gahyun Baek
(Research Institute of Industrial Science and Technology (RIST), Korea)
MES experiments on making methane in zero-gap reactors.



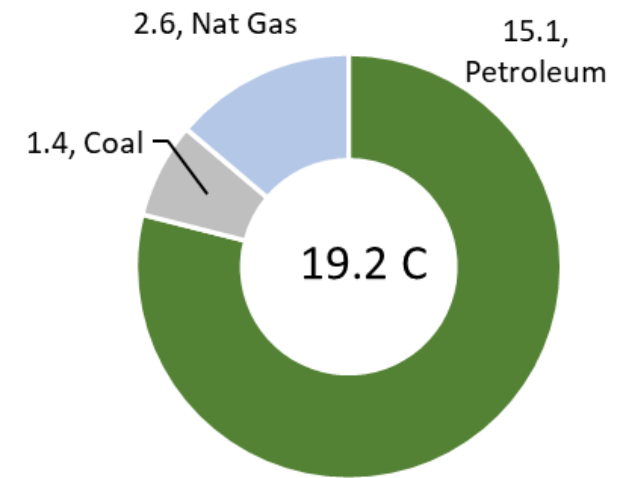
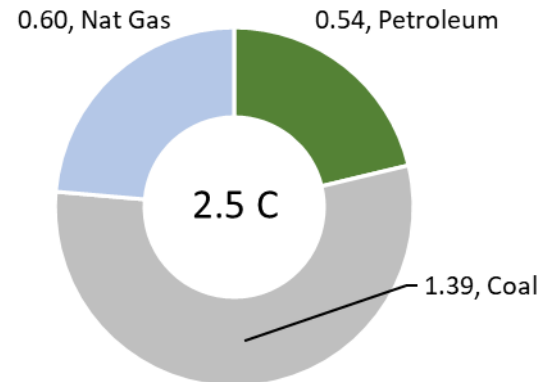
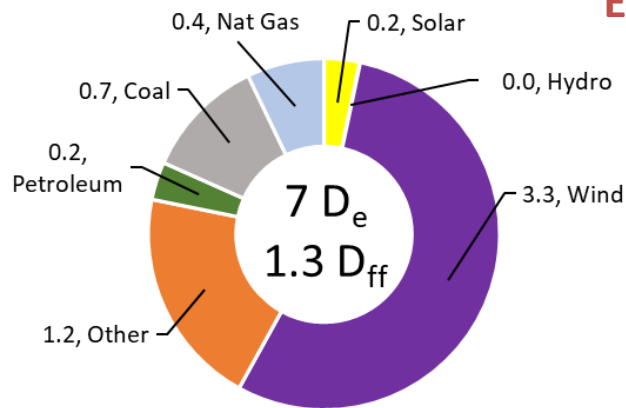
Challenges for Energy in Denmark

- High amount of Petroleum Use
 - 28% of all energy is renewable
 - If you electrify 8.8 D_e replaces 26.3 D_{ff} (assuming 33% fuel to electricity), **total = 19.1 D**
- Energy embedded in the food system
 - Much of the energy consumption is externally consumed (food grown elsewhere)

All Energy



Electricity



Examples of Volumetric Current Densities

| Technology | A_{cat} (m^2/m^3) | I_A (A/m^2) | I_v (A/m^3) | Rate ($\text{kg}/\text{d}\cdot\text{m}^3$) |
|--------------|---|------------------------------------|------------------------------------|---|
| MEC- Reports | 62 | 6.5 | 400 | 0.36 (H_2) |
| - Max | 50 | 50 | 2500 | 2.25 (H_2) |
| MMC- Reports | 5 | 0.11 | 0.55 | 1.6 (CH_4) |
| - Max | 50 | 50 | 2500 | 4.5 (CH_4) |
| MES- Reports | 0.5 | 200 | 100? | 0.54 (acetate) |
| - Max | 100 | 50 | 5000 | 34 (acetate) |

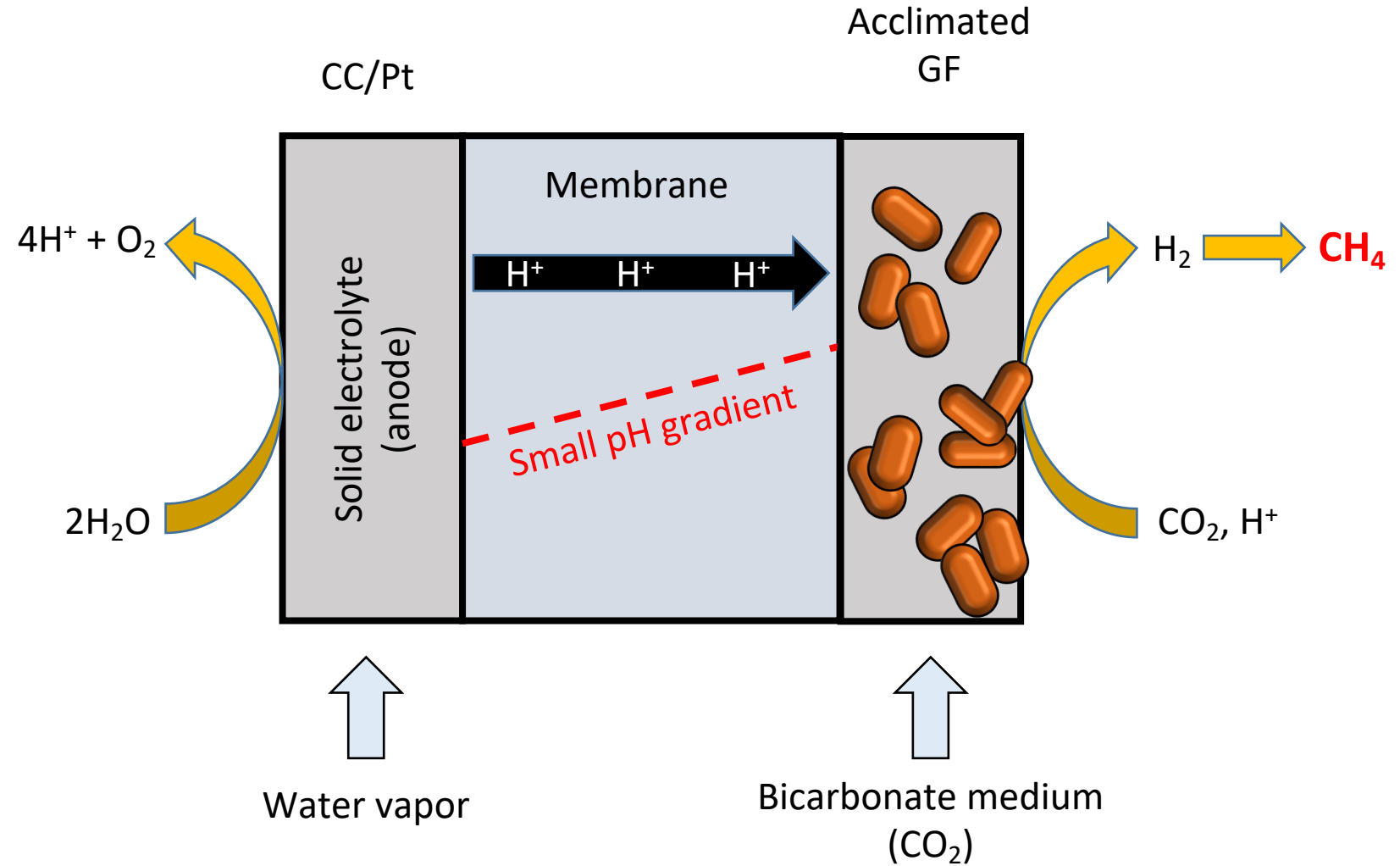
$$1100 \text{ A}/\text{m}^3 = 1 \text{ kg H}_2/\text{d}\cdot\text{m}^3$$

$$1 \text{ kg H}_2 = 2 \text{ kg CH}_4 = 7.5 \text{ kg CH}_3\text{COOH}$$

Examples of Scaling up METs

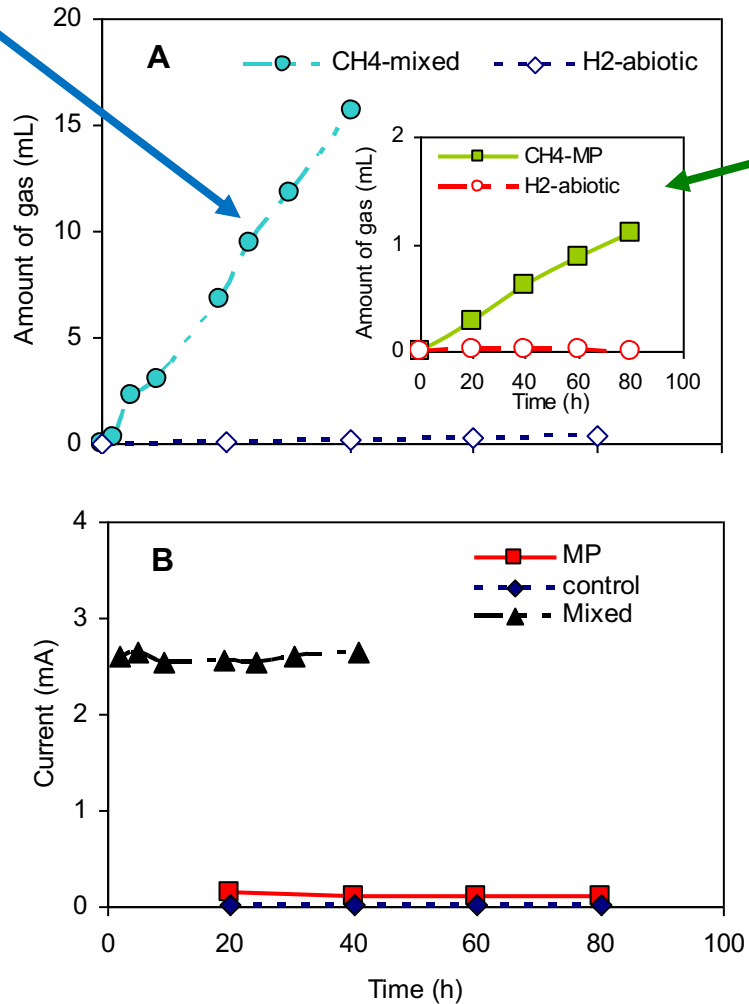
| Technology | Challenges / Opportunities |
|----------------|--|
| MFC | <ul style="list-style-type: none">- Can recover electrical power for particle-free solutions- Wastewater: Maximize current (throw away power) |
| MEC | Electrical power input but H ₂ gas is a valuable product |
| MES/MMC | The “power to gas” technology has great potential and opportunities to inject C-neutral CH ₄ fit into gas pipelines |

New MMC Design: Thin, compact reactors

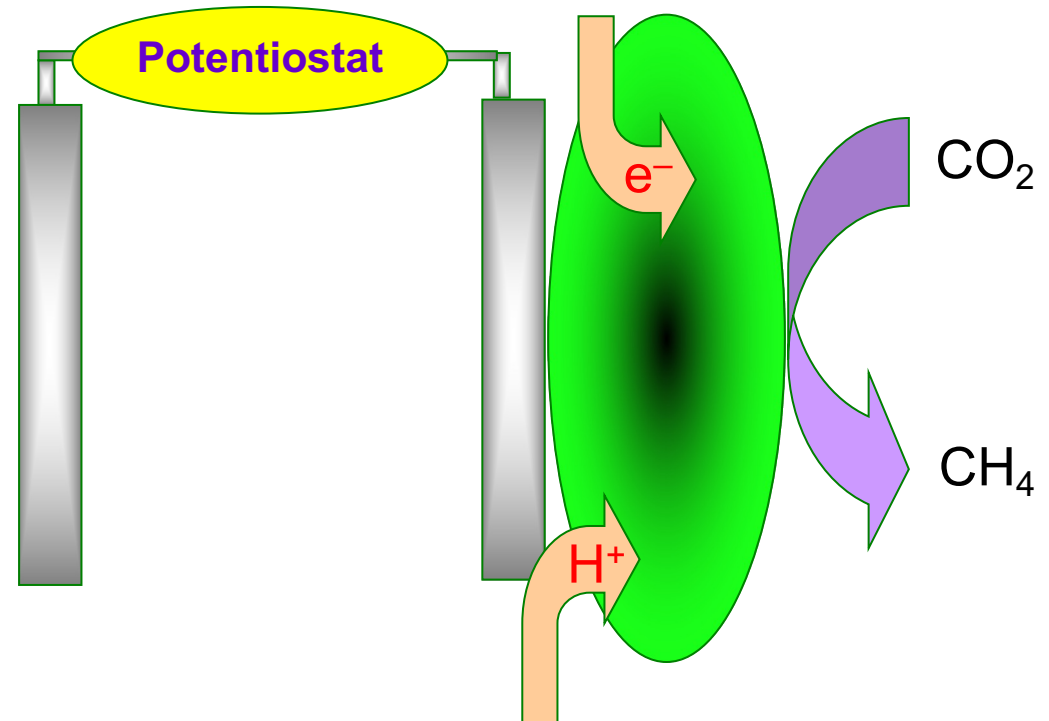


Electrotrophic Methanogens

Mixed culture (*Methanobacterium palustre*)



Pure culture of ATCC *Methanobacterium palustre*



- Water splitting at the anode.
Using Pt. Two phases:

- 1-2: Carbon cloth (degraded)
- 3-6: Titanium

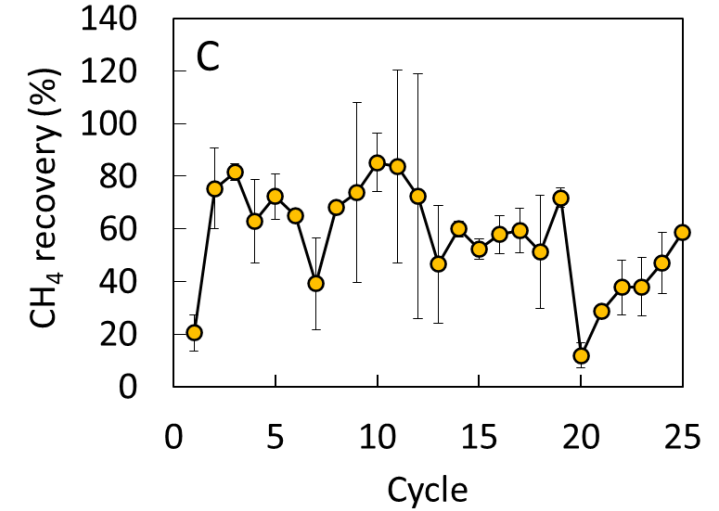
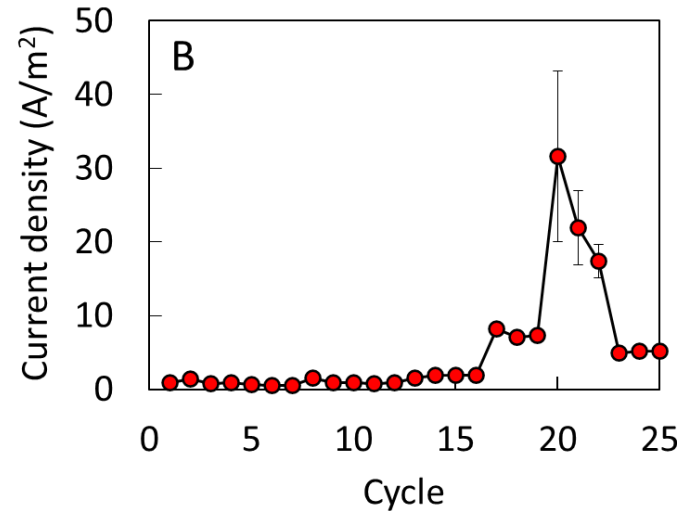
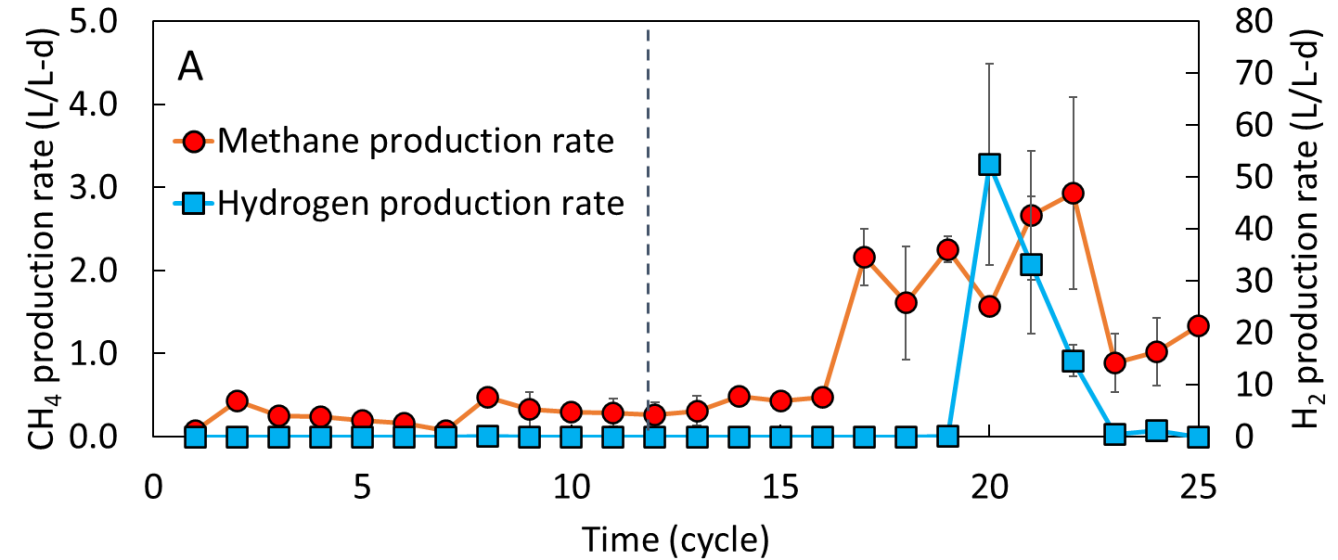
- Increased applied voltages

- 2.0 – 3.1 V
- H₂ measured at 3.1 V
- Returning to 2.5 V showed lower H₂; likely biocathode damage

- Methane recovery: highest with 2.8 V

- ~ 10 A m²
- ~ 2 L/L-d CH₄

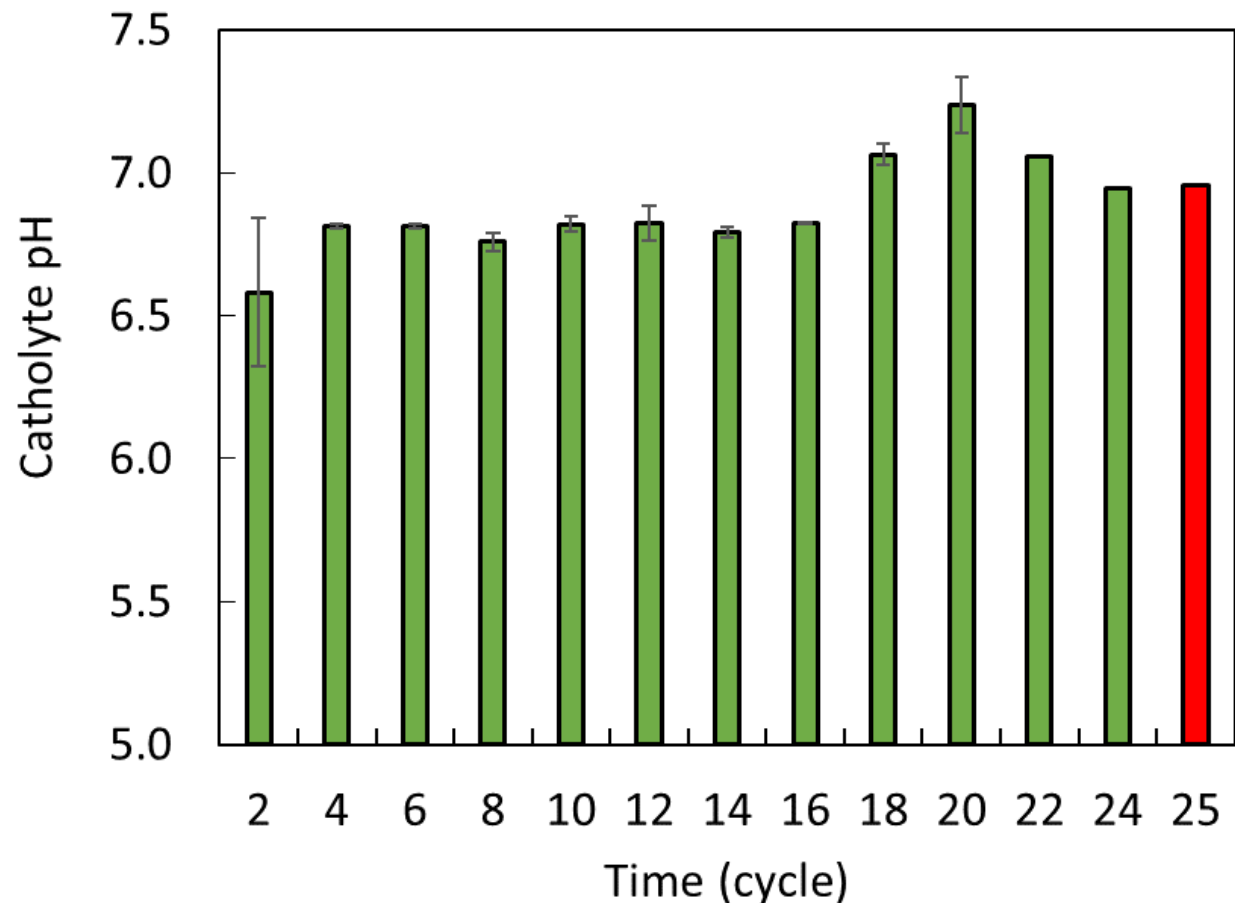
| | Phase 1 | Phase 2 | Phase 3 | Phase 4 | Phase 5 | Phase 6 |
|---------------------|---------|-------------|---------|---------|---------|---------|
| Duration (cycles) | 1–7 | 8–11 | 12–16 | 17–19 | 20–22 | 23–25 |
| Anode material | CC/Pt | CC/Pt (new) | Ti/Pt | Ti/Pt | Ti/Pt | Ti/Pt |
| E _{ap} (V) | 2.0 | 2.0 | 2.5 | 2.8 | 3.1 | 2.8 |



The zero-gap configuration maintains pH

- Need to avoid alkaline catholyte pH
- 1-24 cycles: catholyte switched each cycle (~1-2 d)
 - $6.6 < \text{pH} < 7.2$
- **25th cycle:** extended for 6 days
 - No change in pH

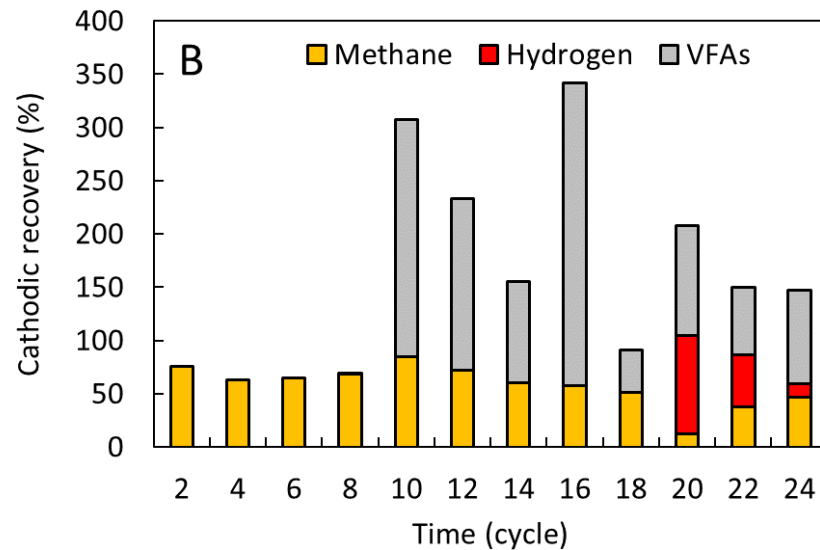
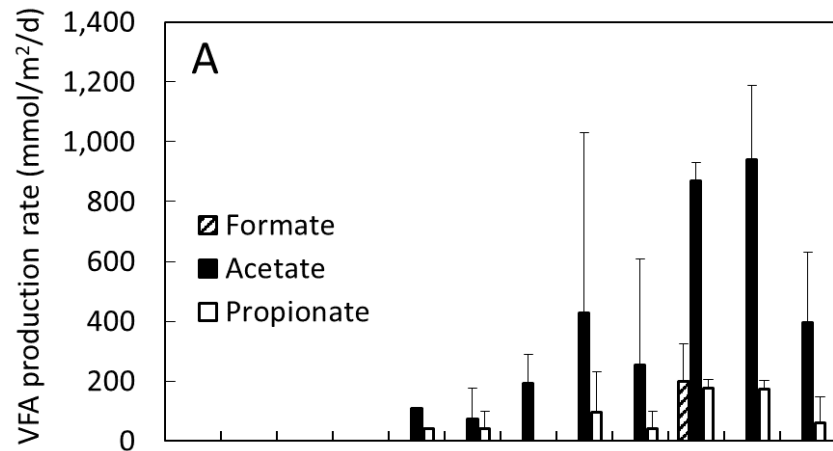
| | Phase 1 | Phase 2 | Phase 3 | Phase 4 | Phase 5 | Phase 6 |
|---------------------|---------|-------------|---------|---------|---------|---------|
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| Anode material | CC/Pt | CC/Pt (new) | Ti/Pt | Ti/Pt | Ti/Pt | Ti/Pt |
| E_{ap} (V) | 2.0 | 2.0 | 2.5 | 2.8 | 3.1 | 2.8 |



VFAs produced in addition to methane

Primarily: Acetate, propionate, formate

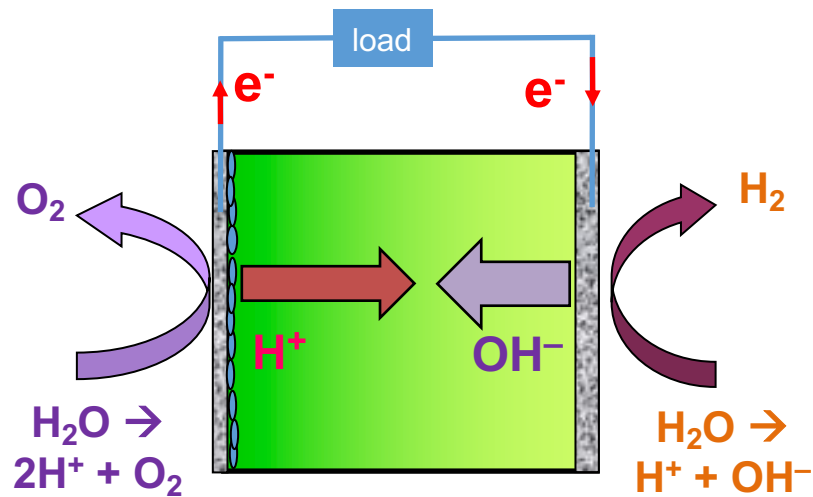
Methanobacteriaceae and Firmicutes



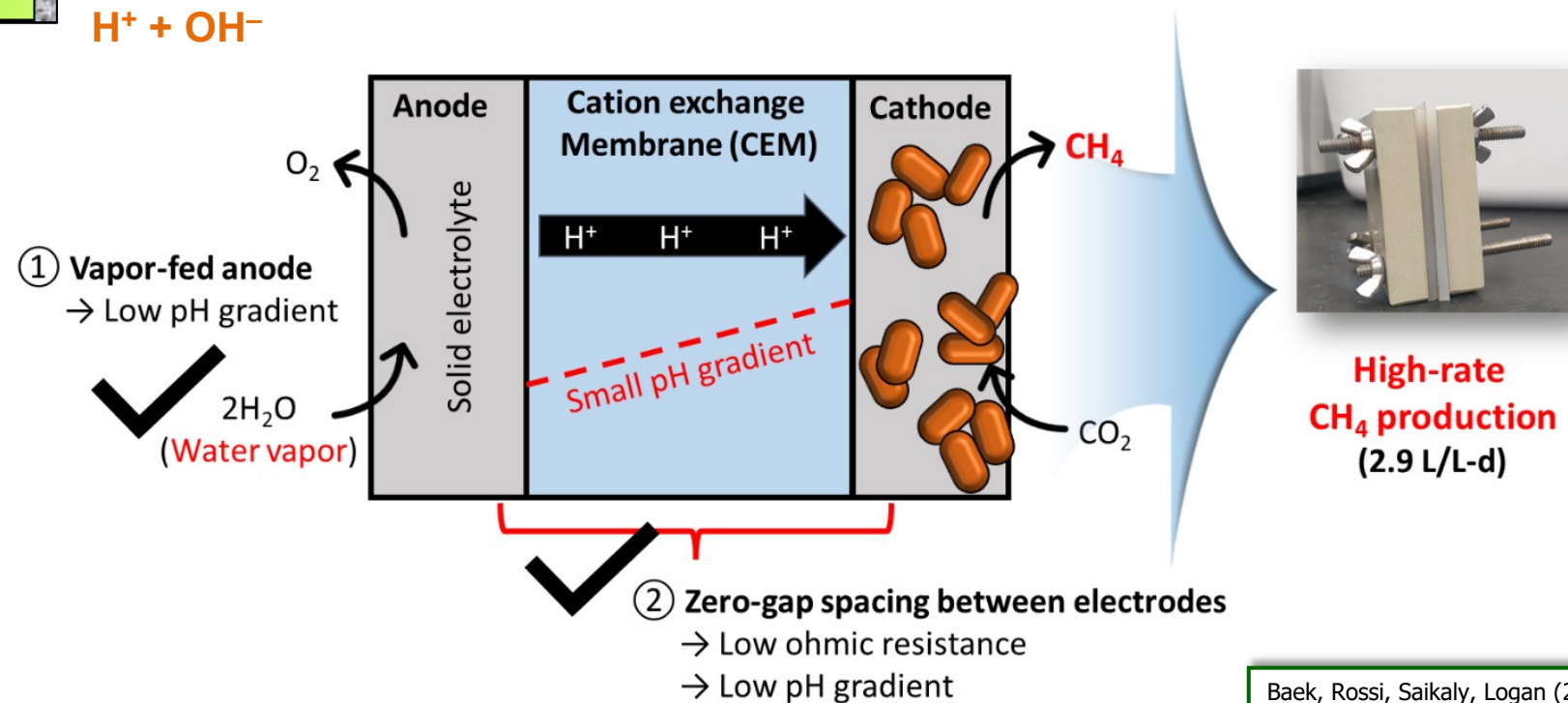
| OTU | Phylum | Family | Genus | MES1 (%) | MES2 (%) | AVG (%) |
|--------|----------------|---------------------|-----------------------------|----------|----------|---------|
| OTU 1 | Euryarchaeota | Methanobacteriaceae | Methanobrevibacter | 32.5 | 38.8 | 35.7 |
| OTU 2 | Firmicutes | Clostridiaceae 1 | Clostridium sensu stricto 1 | 12.4 | 9.4 | 10.9 |
| OTU 3 | Firmicutes | Eubacteriaceae | Eubacterium | 12.7 | 3.6 | 8.2 |
| OTU 4 | Bacteroidetes | Rikenellaceae | - | 7.0 | 9.3 | 8.1 |
| OTU 5 | Proteobacteria | Rhodocyclaceae | Azospira | 4.0 | 12.1 | 8.0 |
| OTU 6 | Proteobacteria | Pseudomonadaceae | Pseudomonas | 6.5 | 3.5 | 5.0 |
| OTU 7 | Proteobacteria | Burkholderiaceae | Alcaligenes | 4.1 | 3.6 | 3.8 |
| OTU 8 | Actinobacteria | Nocardiaceae | Gordonia | 1.6 | 2.6 | 2.1 |
| OTU 9 | Firmicutes | Lachnospiraceae | Tyzzarella | 1.8 | 1.7 | 1.7 |
| OTU 10 | Euryarchaeota | Methanobacteriaceae | Methanobrevibacter | 2.0 | 1.0 | 1.5 |



MES: Methane Generation by Water Splitting & Biocathodes



- H^+ produced with O_2 by water splitting anode
- A **CEM** is used for MES (Not an AEM that is used in MFC or MEC) to facilitate H^+ transport



- Water splitting at the anode.

- Using Pt. Two phases:

- 1-2: Carbon cloth (degraded)
- 3-6: Titanium

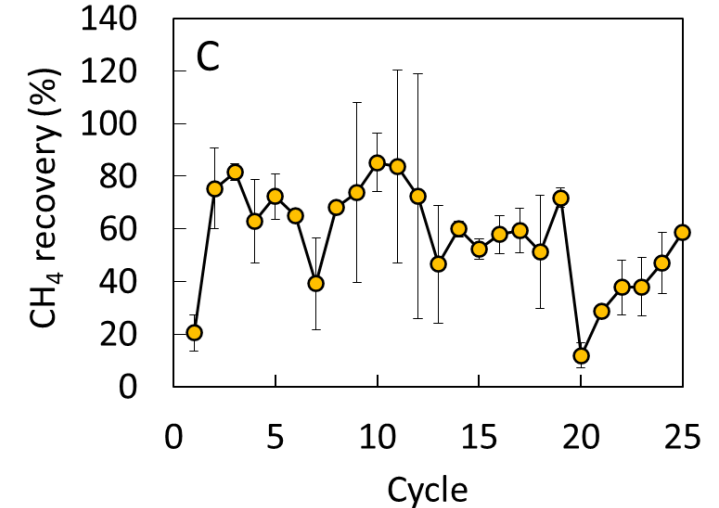
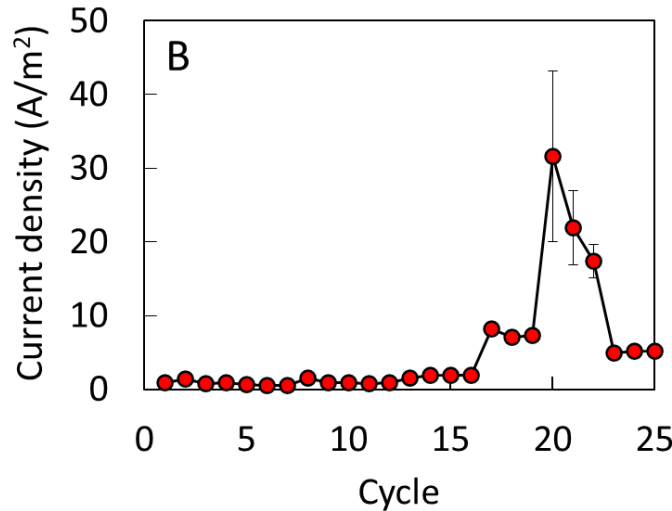
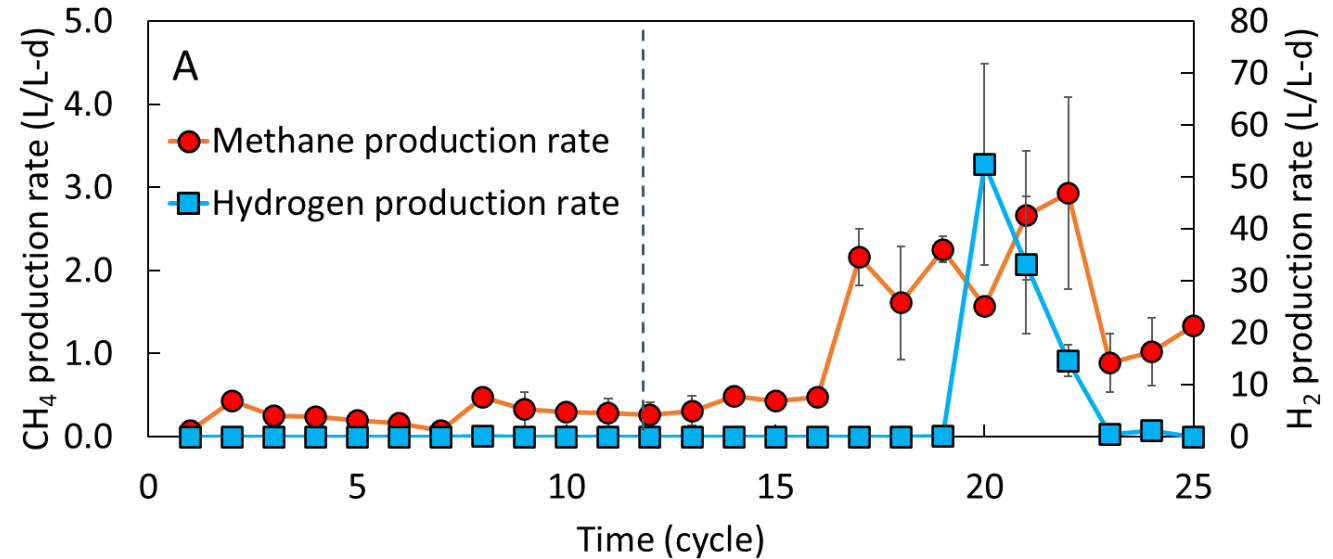
- Increased applied voltages

- 2.0 – 3.1 V
- 3.1 V too high (H_2 measured)

- Methane recovery:

- Highest at 2.8 V
- 2 L/L-d CH_4 ($10 A m^2$)

| | Phase 1 | Phase 2 | Phase 3 | Phase 4 | Phase 5 | Phase 6 |
|-------------------|---------|-------------|---------|---------|---------|---------|
| Duration (cycles) | 1–7 | 8–11 | 12–16 | 17–19 | 20–22 | 23–25 |
| Anode material | CC/Pt | CC/Pt (new) | Ti/Pt | Ti/Pt | Ti/Pt | Ti/Pt |
| E_{ap} (V) | 2.0 | 2.0 | 2.5 | 2.8 | 3.1 | 2.8 |




Does adding electrodes into AD work?

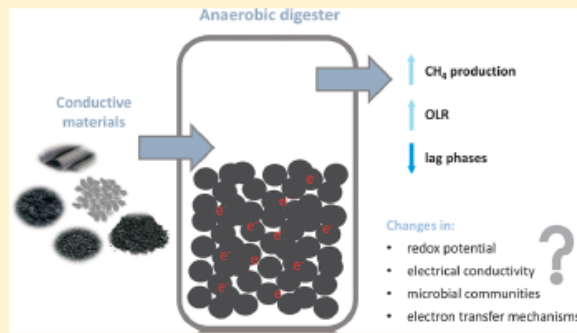
Methane Production and Conductive Materials: A Critical Review

Gilberto Martins,^{*✉} Andreia F. Salvador, Luciana Pereira, and M. Madalena Alves

Centre of Biological Engineering, University of Minho, Campus de Gualtar, 4710-057 Braga, Portugal

 Supporting Information

ABSTRACT: Conductive materials (CM) have been extensively reported to enhance methane production in anaerobic digestion processes. The occurrence of direct interspecies electron transfer (DIET) in microbial communities, as an alternative or complementary to indirect electron transfer (via hydrogen or formate), is the main explanation given to justify the improvement of methane production. Not disregarding that DIET can be promoted in the presence of certain CM, it surely does not explain all the reported observations. In fact, in methanogenic environments DIET was only unequivocally demonstrated in cocultures of *Geobacter metallireducens* with *Methanosaeta harundinacea* or *Methanosarcina barkeri* and frequently *Geobacter* sp. are not detected in improved methane production driven systems. Furthermore, conductive carbon nanotubes were shown to accelerate the activity of methanogens growing in pure cultures, where DIET is not expected to occur, and hydrogenotrophic activity is ubiquitous in full-scale anaerobic digesters treating for example brewery wastewaters, indicating that interspecies hydrogen transfer is an important electron transfer mechanism in those systems. This paper presents an overview of the effect of several iron-based and carbon-based CM in bioengineered systems, focusing on the improvement in methane production and in microbial communities' changes. Control assays, as fundamental elements to support major conclusions in reported experiments, are critically revised and discussed.



Interfacing anaerobic digestion with (bio)electrochemical systems: Potentials and challenges

Jo De Vrieze^{a,1}, Jan B.A. Arends^{a,1}, Kristof Verbeeck^{a,1}, Sylvia Gildemyn^{a,b}, Korneel Rabaey^{a,*}

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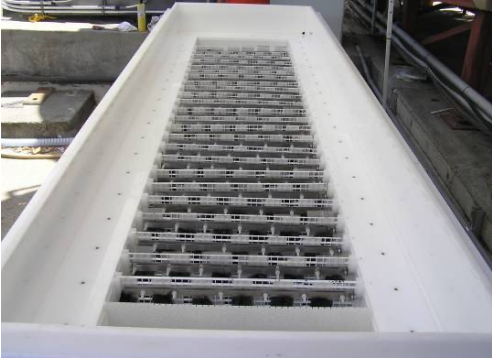
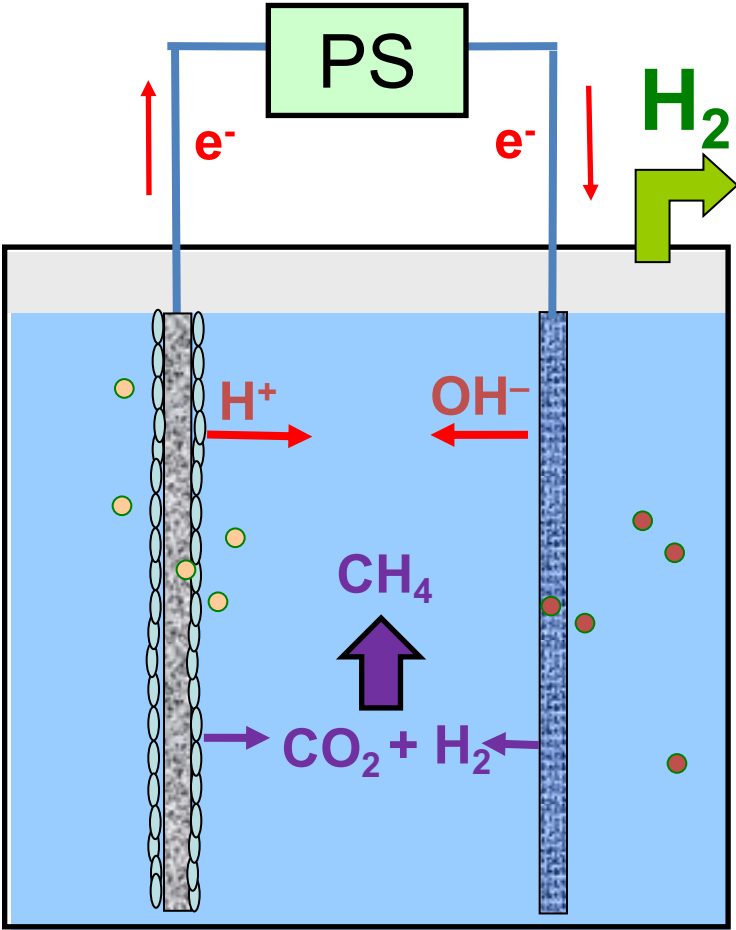
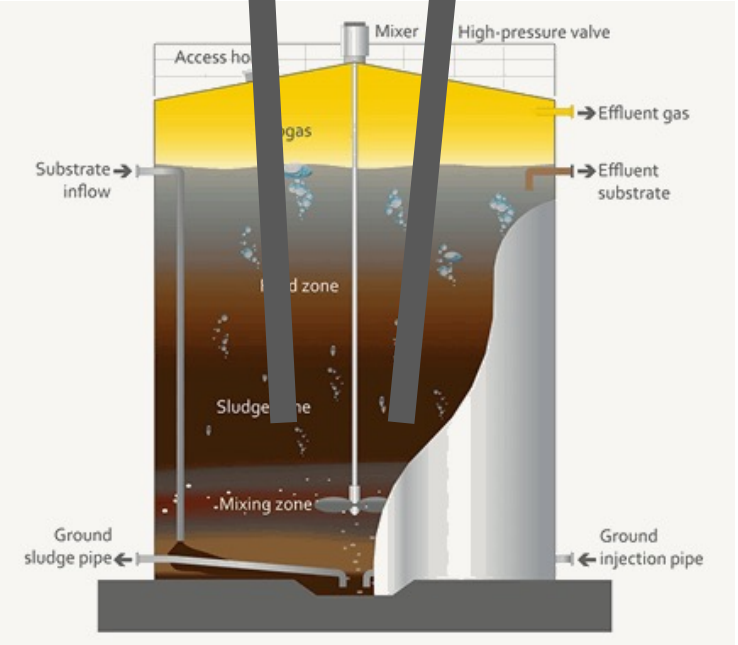
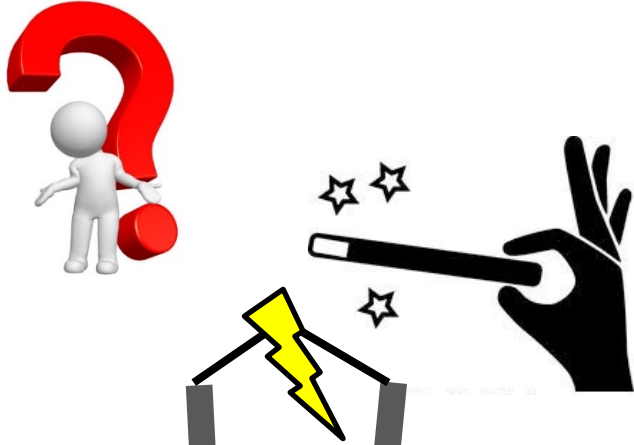
Keywords:
Anaerobic digestion
Bioelectrochemical system
Biogas
Methane
Resource recovery

ABSTRACT

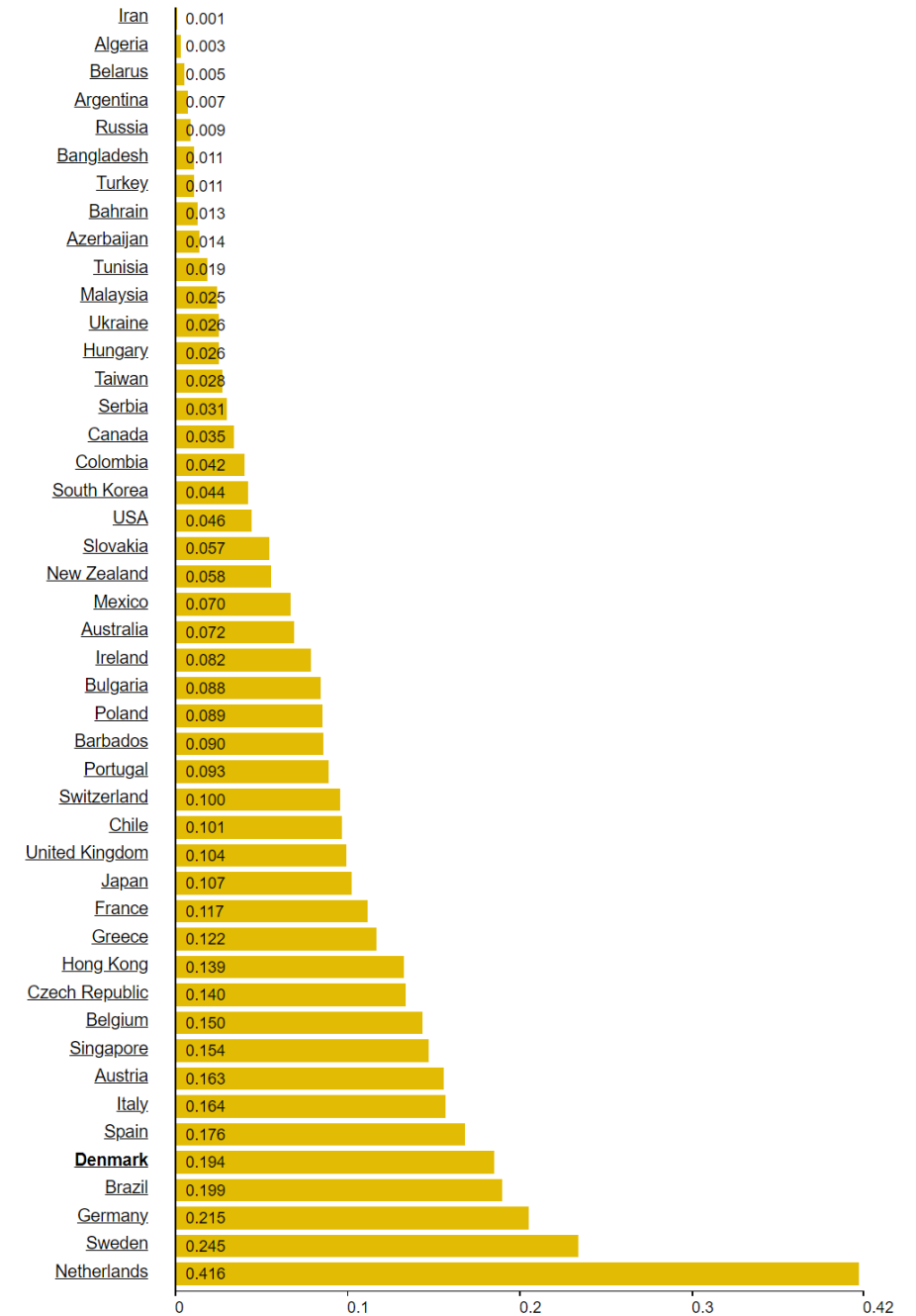
For over a century, anaerobic digestion has been a key technology in stabilizing organic waste streams, while at the same time enabling the recovery of energy. The anticipated transition to a bio-based economy will only increase the quantity and diversity of organic waste streams to be treated, and, at the same time, increase the demand for additional and effective resource recovery schemes for nutrients and organic matter. The performance of anaerobic digestion can be supported and enhanced by (bio) electrochemical systems in a wide variety of hybrid technologies. Here, the possible benefits of combining anaerobic digestion with (bio)electrochemical systems were reviewed in terms of (1) process monitoring, control, and stabilization, (2) nutrient recovery, (3) effluent polishing, and (4) biogas upgrading. The interaction between microorganisms and electrodes with respect to niche creation is discussed, and the potential impact of this interaction on process performance is evaluated. The strength of combining anaerobic digestion with (bio)electrochemical technologies resides in the complementary character of both technologies, and this perspective was used to distinguish transient trends from schemes with potential for full-scale application. This is supported by an operational costs assessment, showing that the economic potential of combining anaerobic digestion with a (bio)electrochemical system is highly case-specific, and strongly depends on engineering challenges with respect to full-scale applications.

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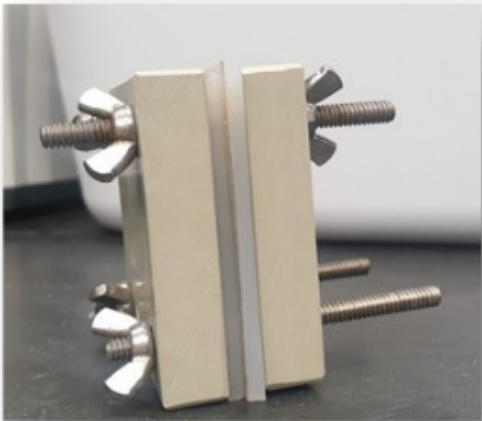
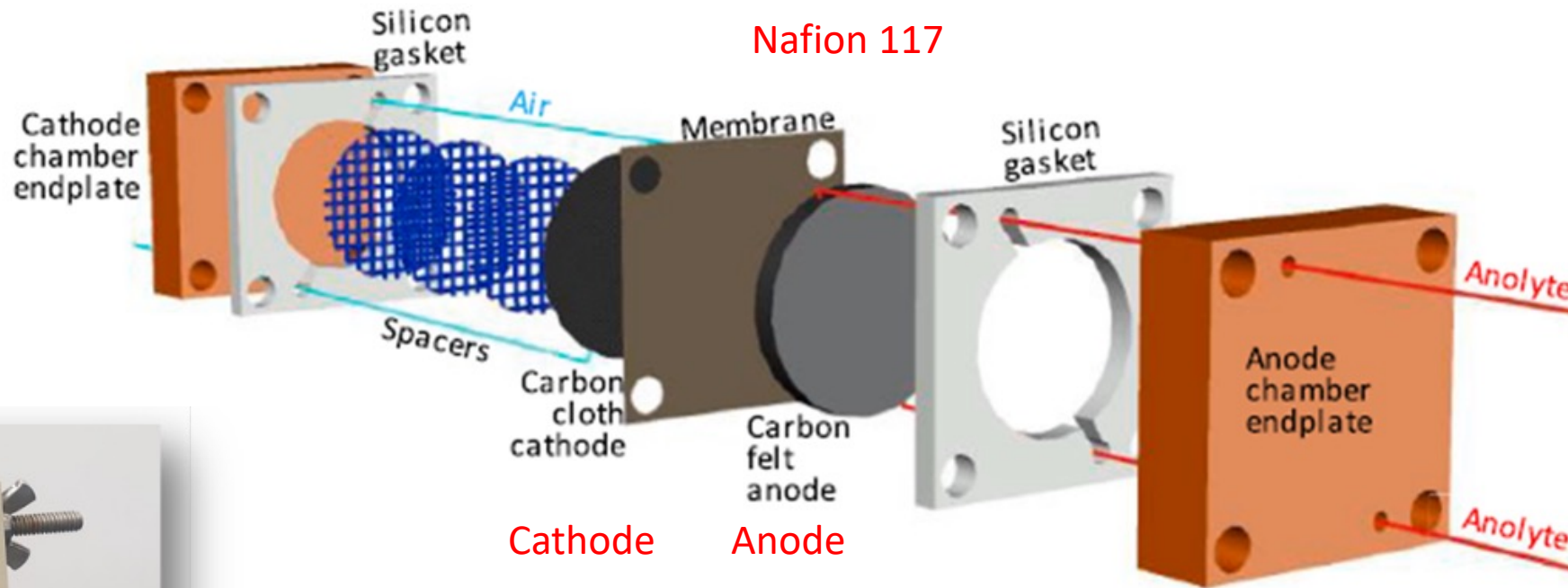
Using MECs for Enhanced Anaerobic Digestion?



Natural gas prices for households, March 2022
(kWh, U.S. Dollar)



Water-splitting MMCs have not been scaled up ...



There can be many of these cell pairs in a stack.
Just one cell pair shown here

